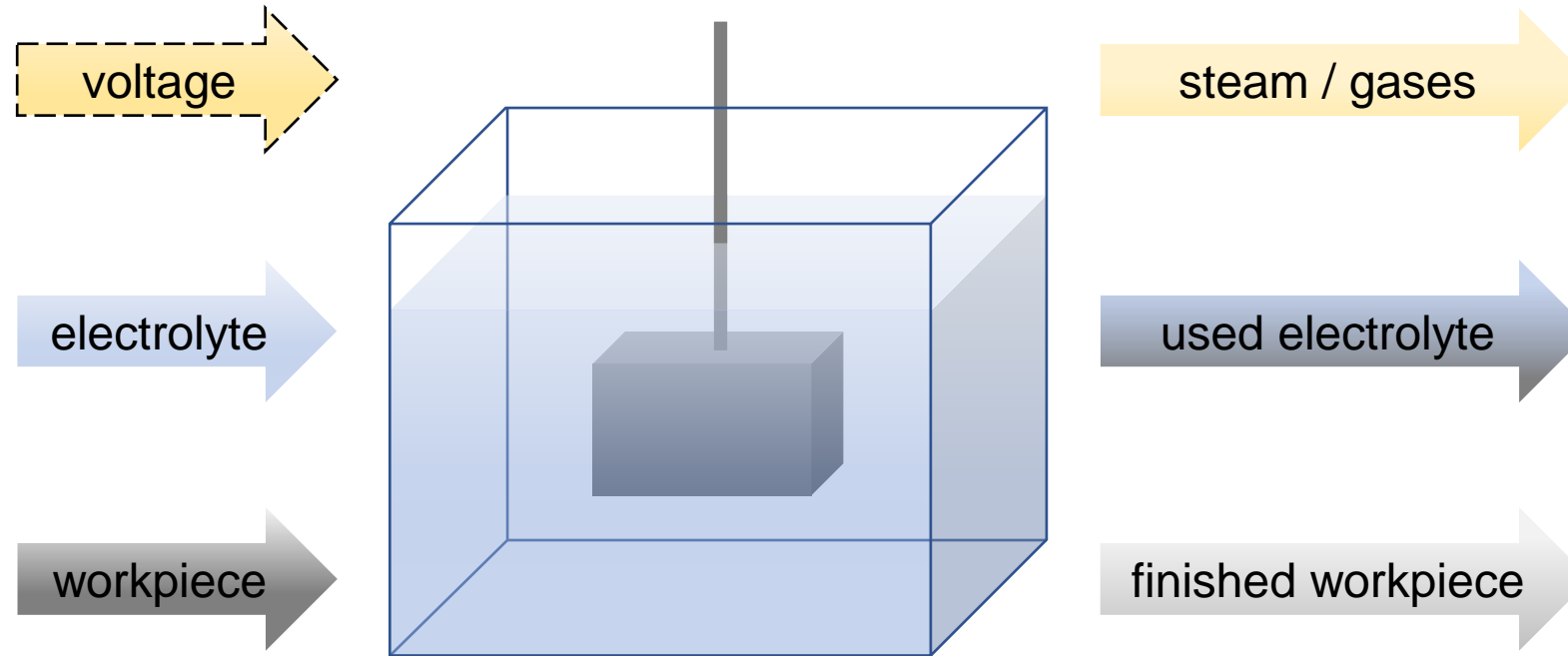


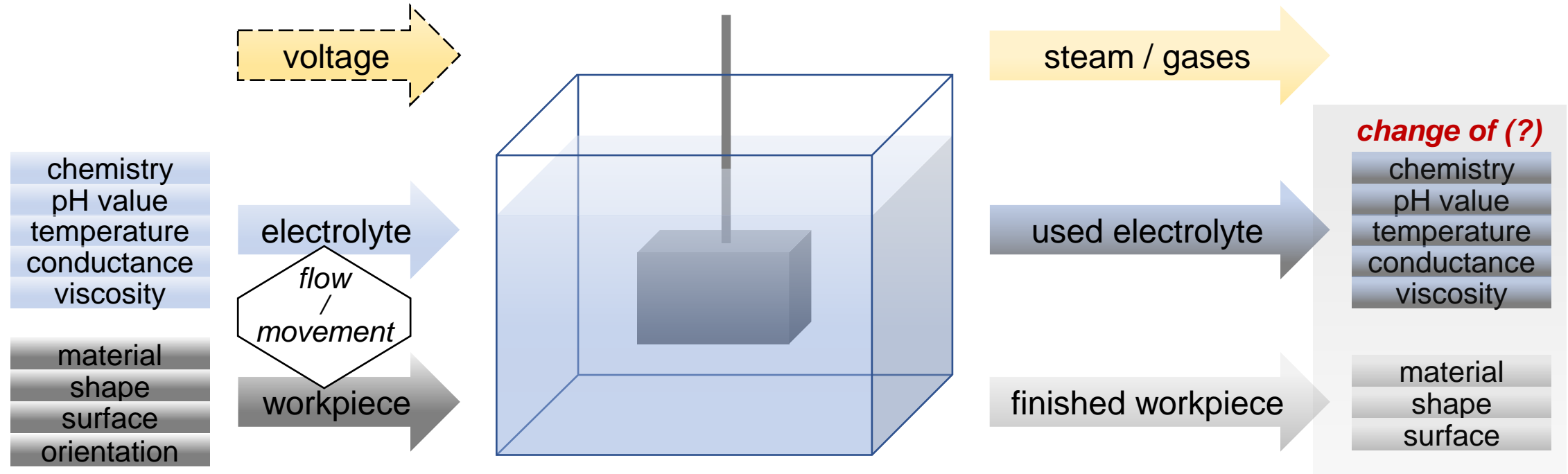
# UNDERSTANDING PEP

## Part 1: Mechanisms, Chemistry, Parameters

# Understanding Pep

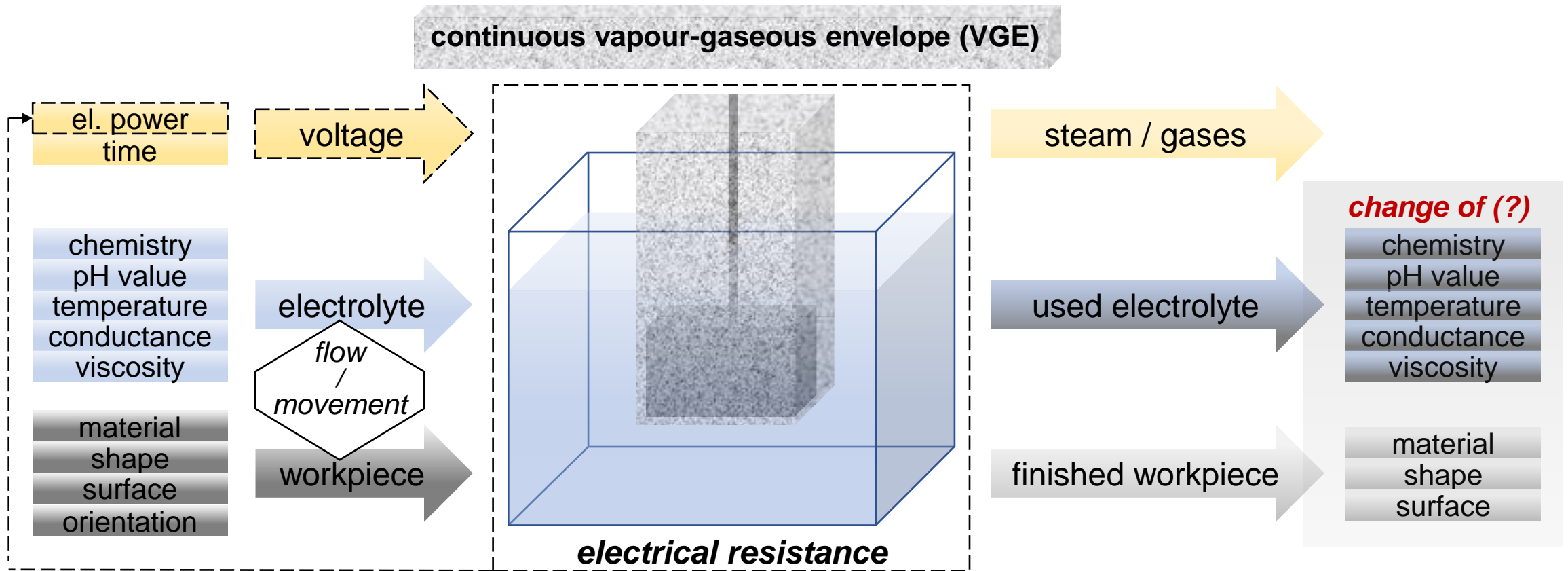


# Understanding Pep



**(not) a simple process with complex relations?!**

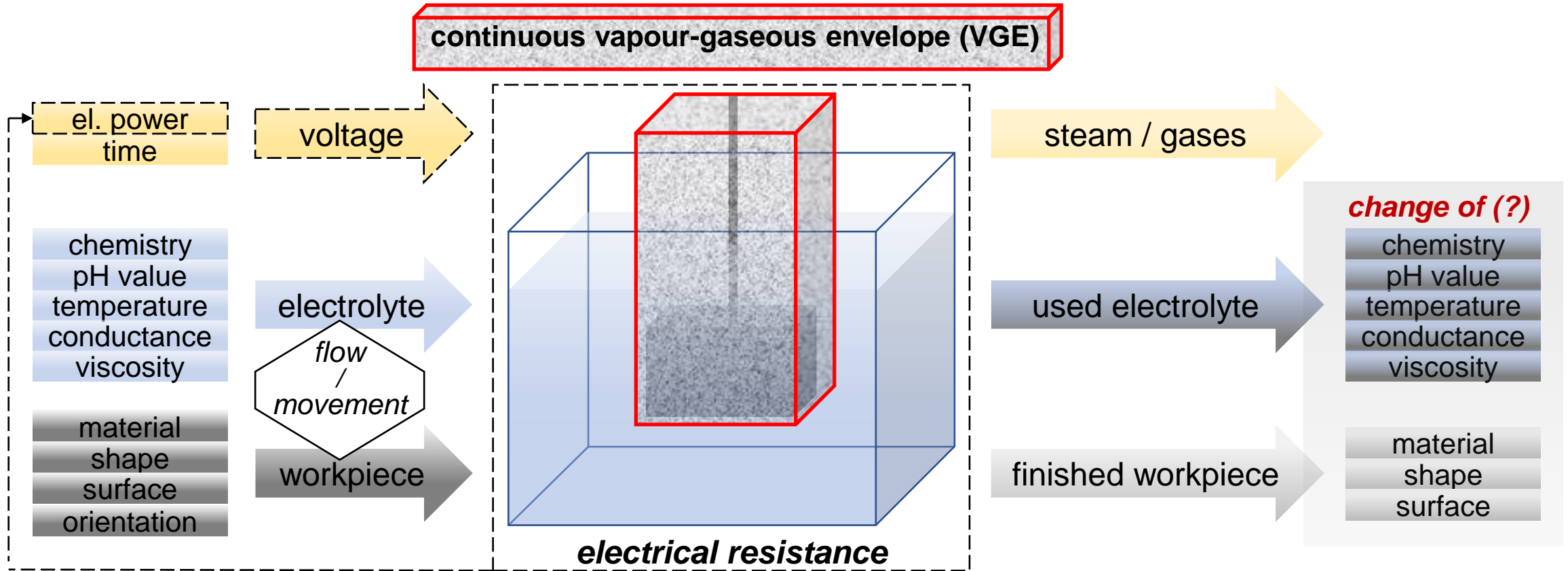
# Understanding Pep



**Special feature:** Plasma forms under atmospheric pressure in liquid

# Understanding Pep

# vapour-gaseous envelope (VGE)

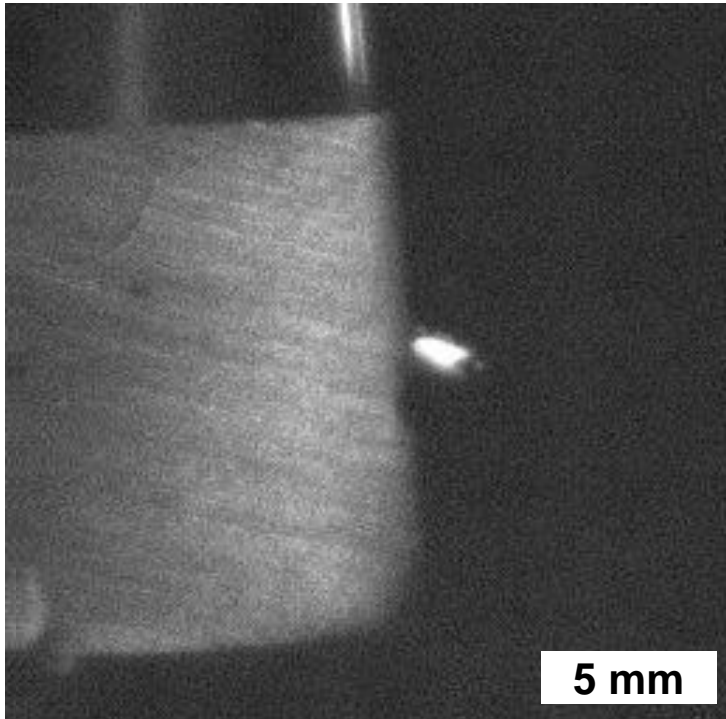


(not) a simple process with complex relations?!

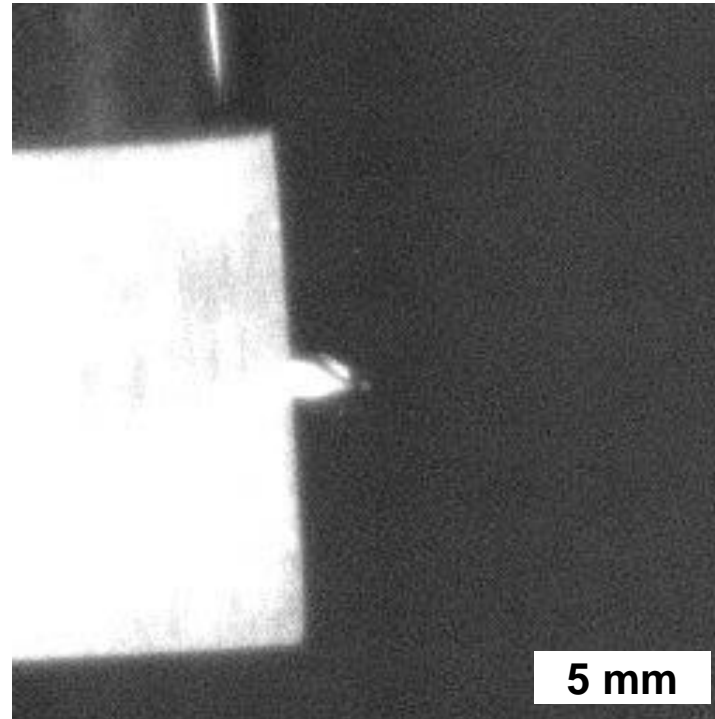
# Understanding Pep

# Developement of VGE

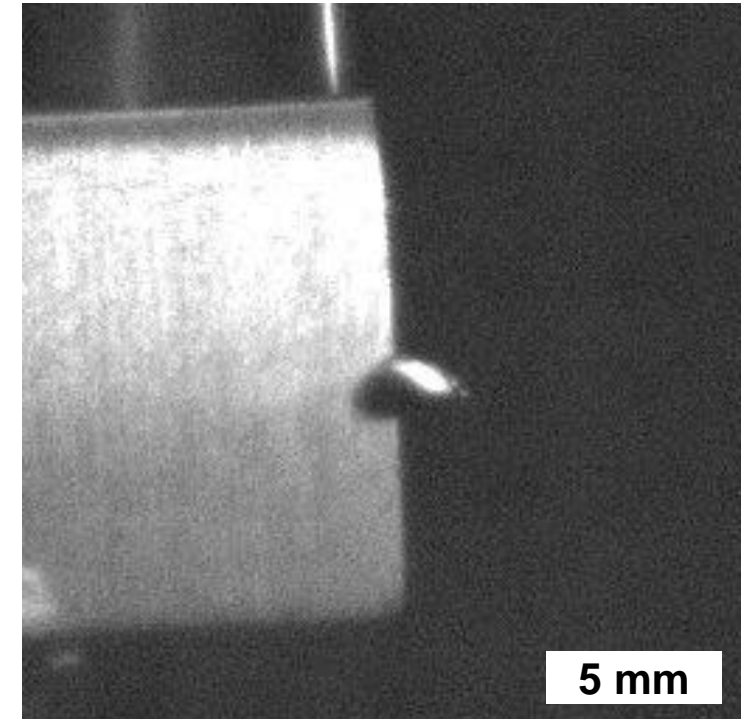
High-speed Camera recordings starting submerged: **0.0 ms  $\leq$  t  $\leq$  8.33 ms**



316 V



340 V



360 V

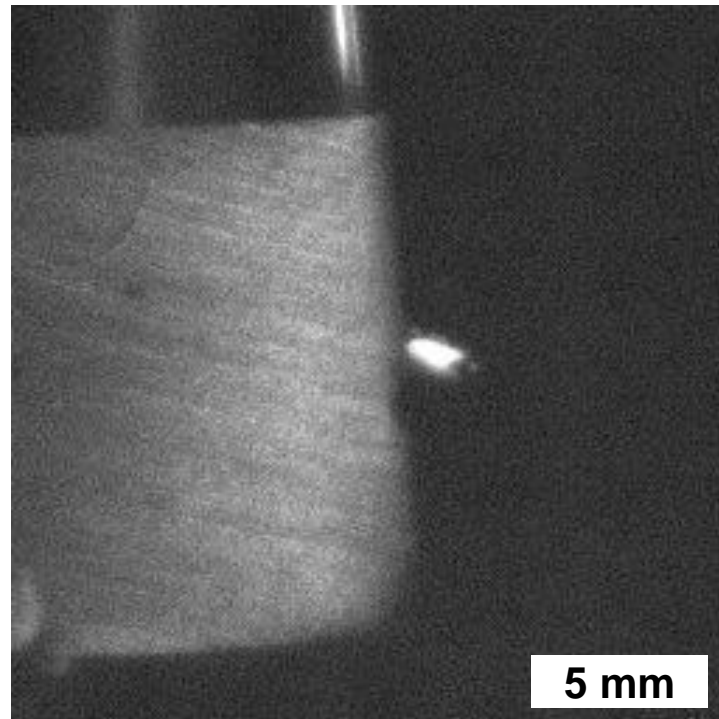
→ Very fast and high hydrodynamic process

# Understanding Pep

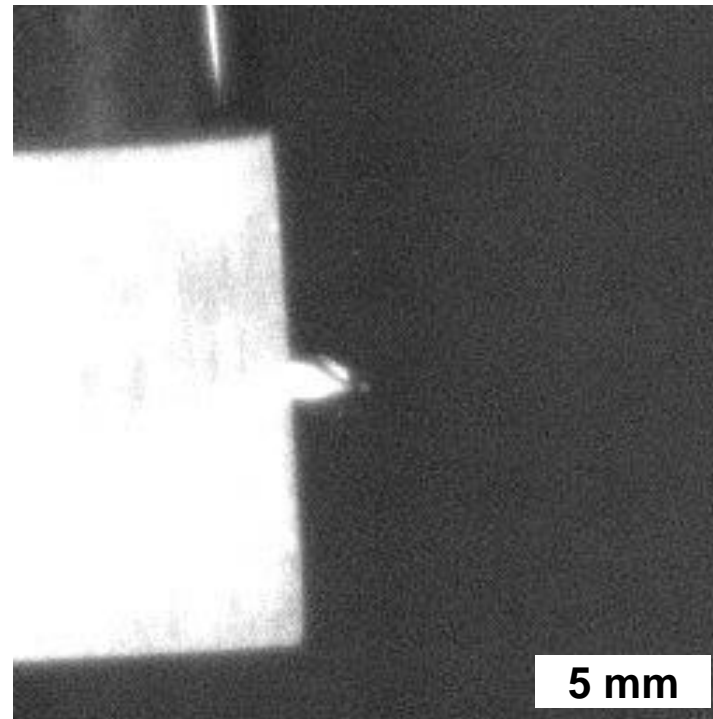
# Developement of VGE

High-speed Camera recordings starting submerged:  **$0.0 \text{ ms} \leq t \leq 8.33 \text{ ms}$**

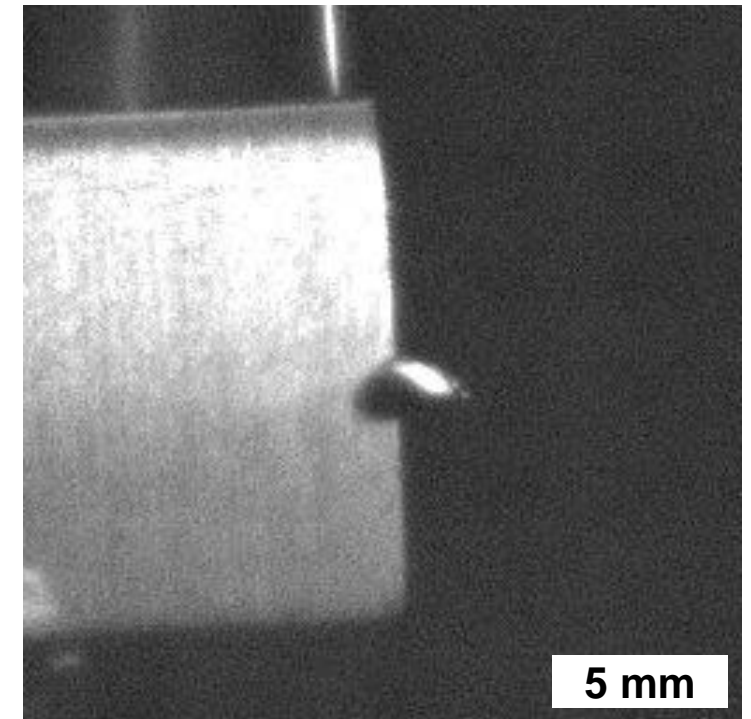
**$\rightarrow t = 0 \text{ ms}$**



316 V



340 V



360 V

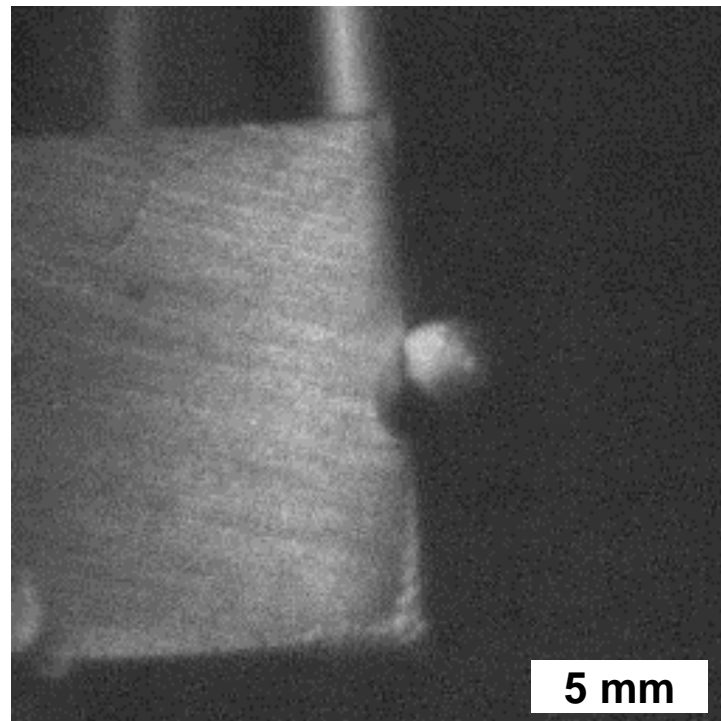
**$\rightarrow$  Very fast and high hydrodynamic process**

# Understanding Pep

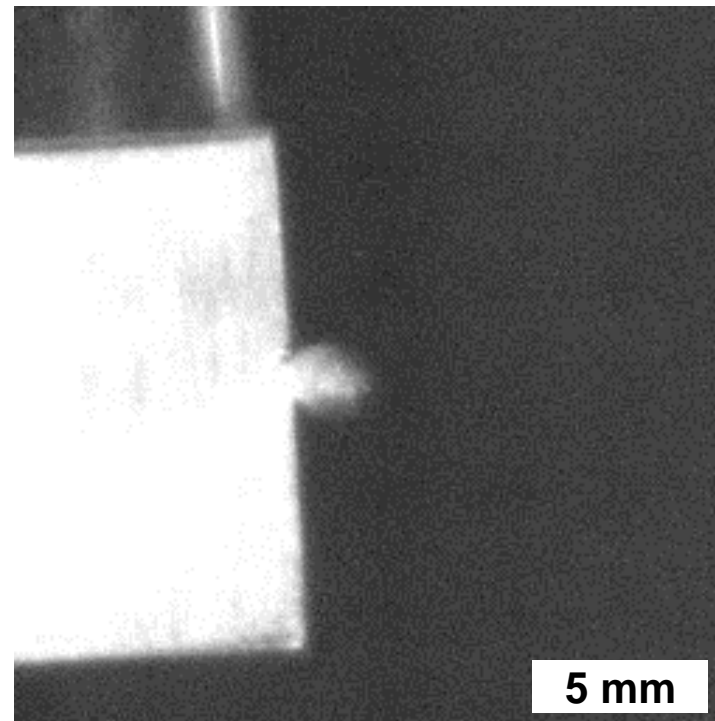
# Developement of VGE

High-speed Camera recordings starting submerged:  $0.0 \text{ ms} \leq t \leq 8.33 \text{ ms}$

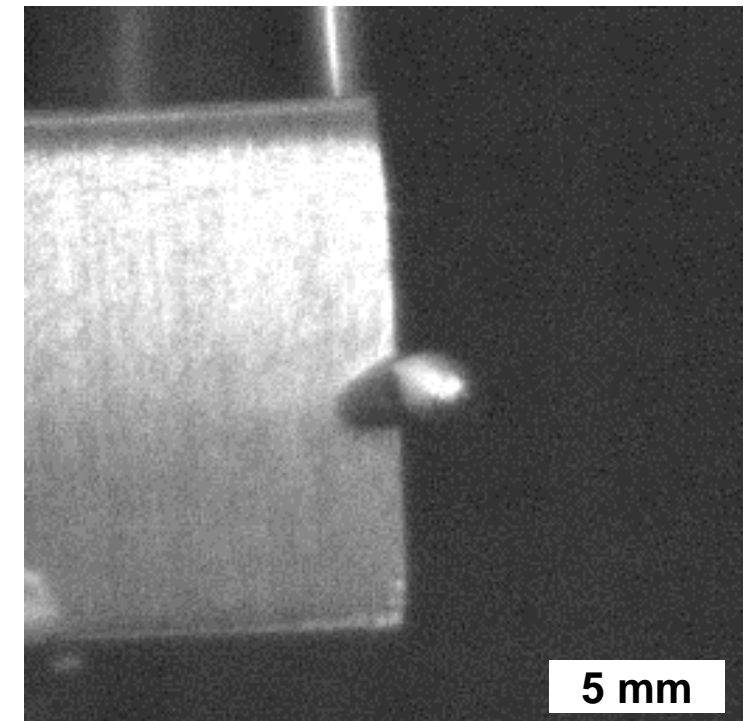
→  $t = 0.33 \text{ ms}$



316 V



340 V



360 V

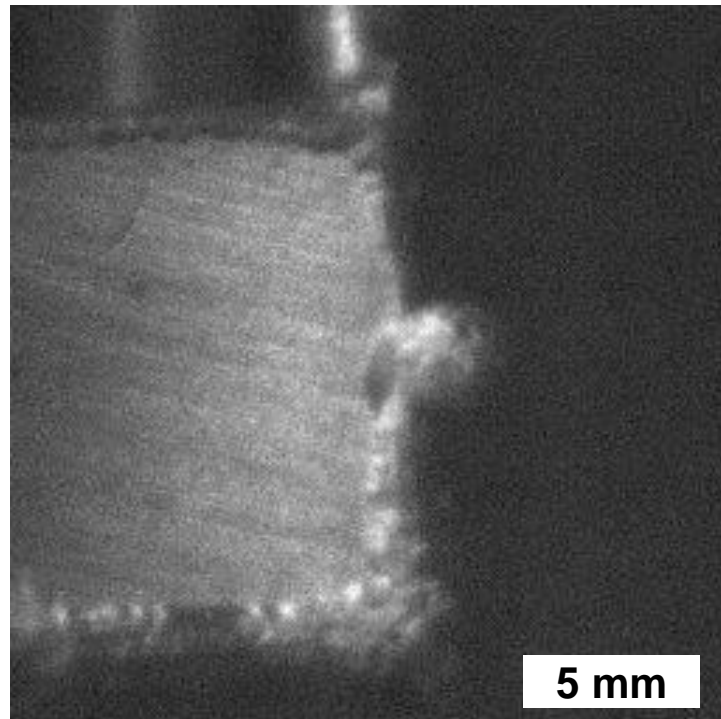
→ Very fast and high hydrodynamic process

# Understanding Pep

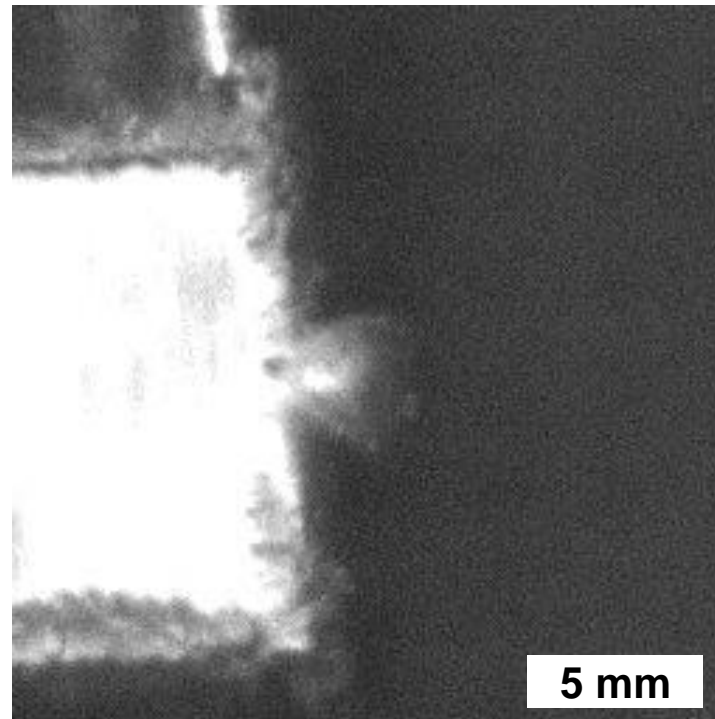
# Developement of VGE

High-speed Camera recordings starting submerged:  **$0.0 \text{ ms} \leq t \leq 8.33 \text{ ms}$**

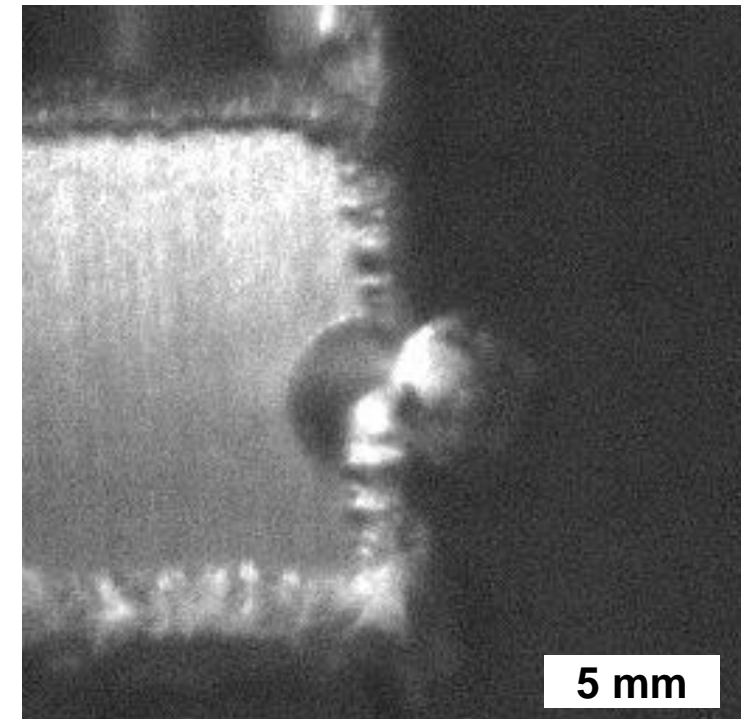
**$\rightarrow t = 1 \text{ ms}$**



316 V



340 V



360 V

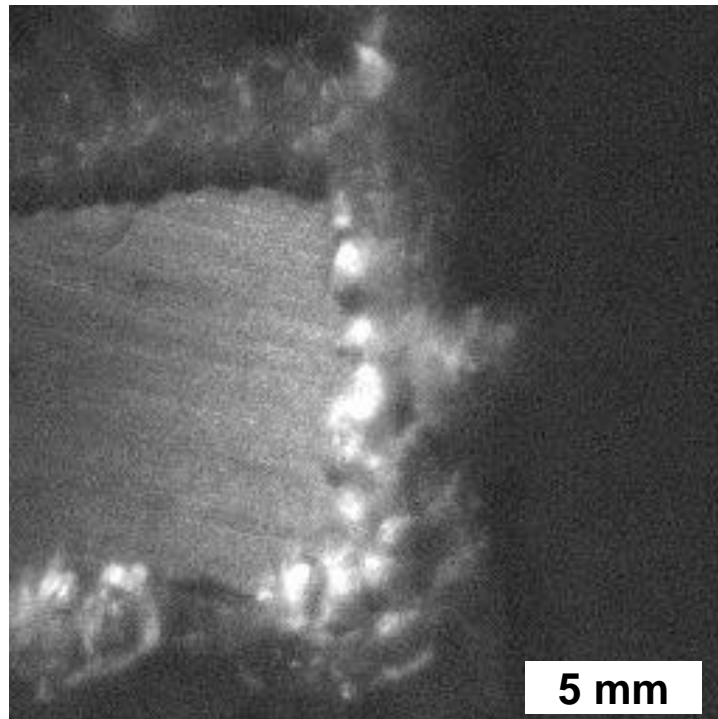
**$\rightarrow$  Very fast and high hydrodynamic process**

# Understanding Pep

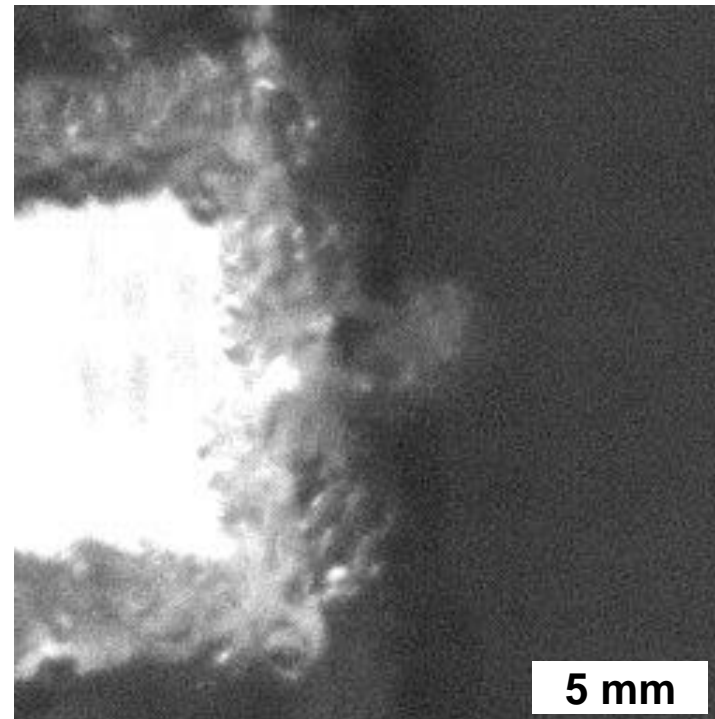
# Developement of VGE

High-speed Camera recordings starting submerged: **0.0 ms  $\leq$  t  $\leq$  8.33 ms**

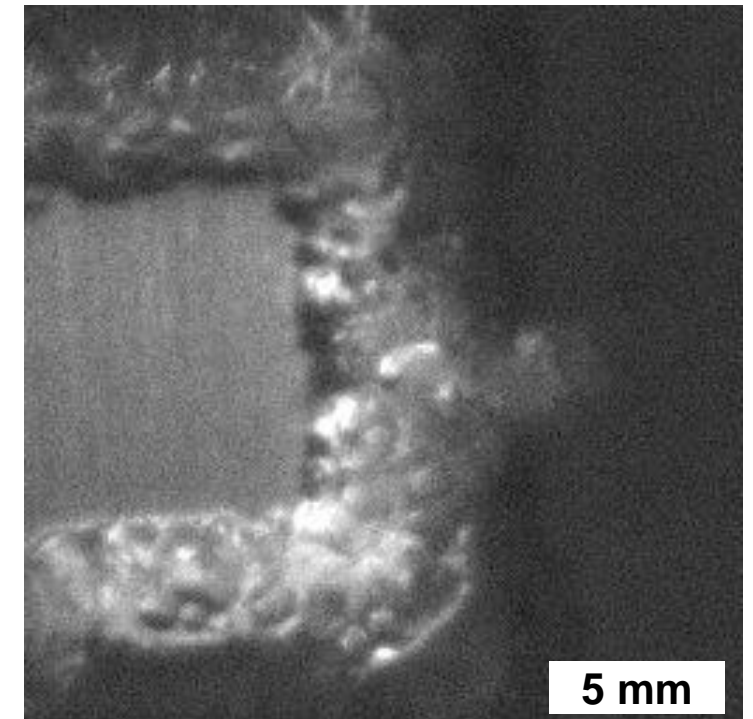
**$\rightarrow$  t = 2 ms**



316 V



340 V



360 V

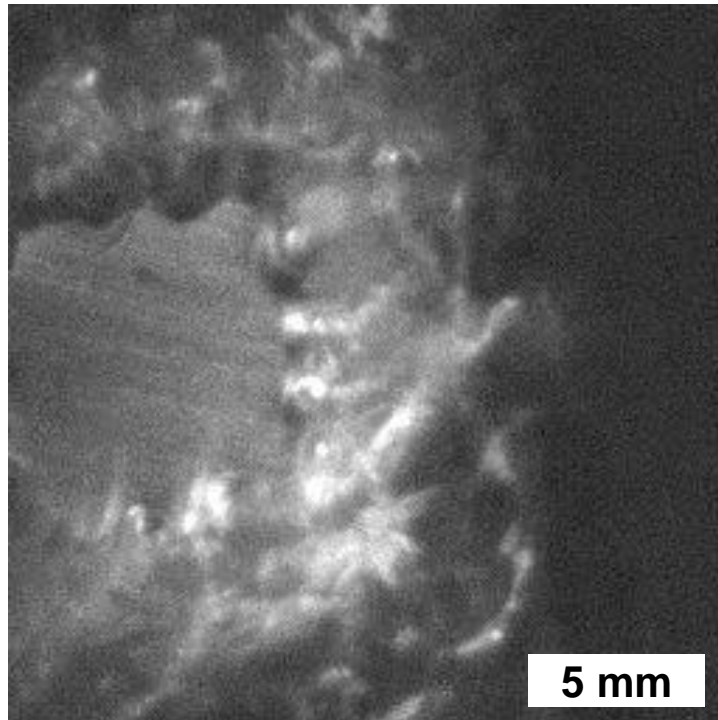
**$\rightarrow$  Very fast and high hydrodynamic process**

# Understanding Pep

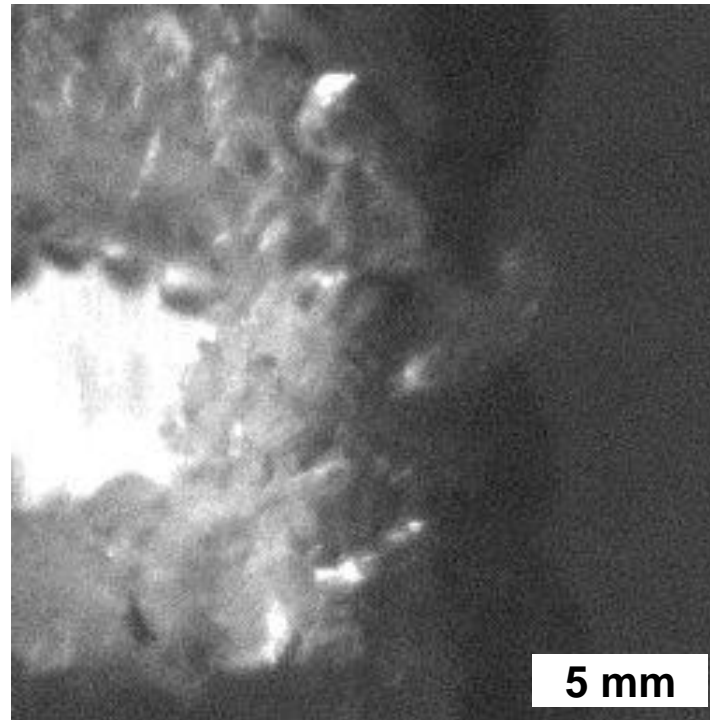
# Developement of VGE

High-speed Camera recordings starting submerged:  $0.0 \text{ ms} \leq t \leq 8.33 \text{ ms}$

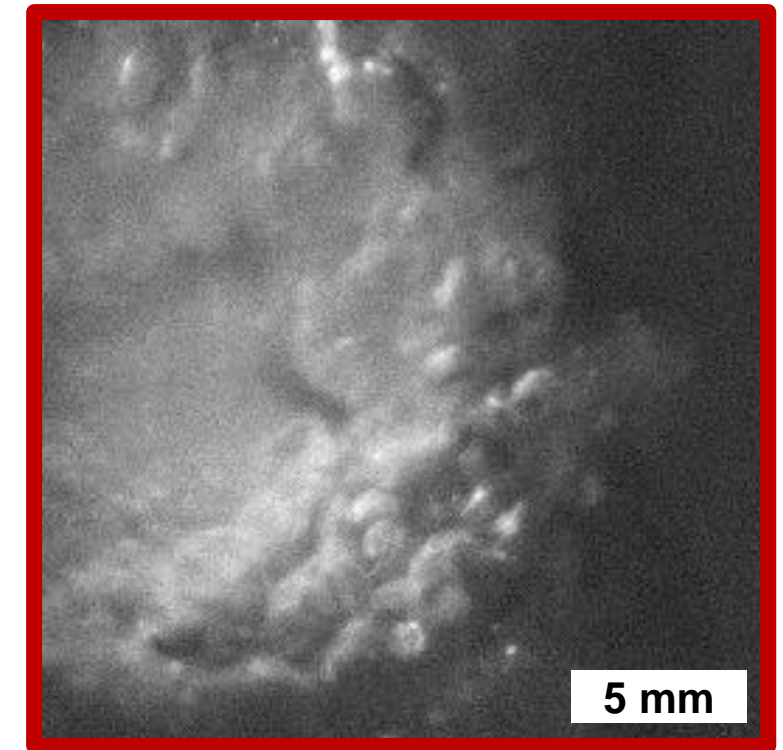
→  $t = 3.17 \text{ ms}$



316 V



340 V



360 V

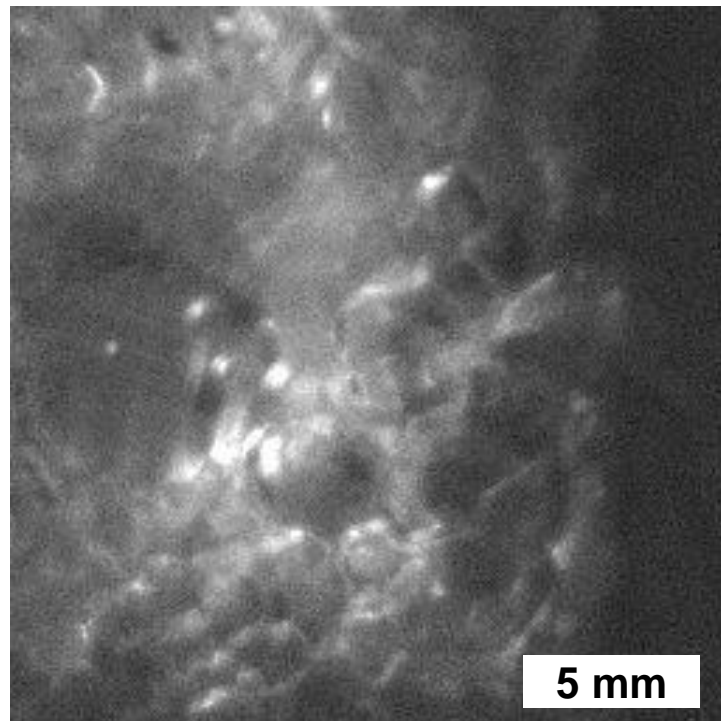
→ Very fast and high hydrodynamic process

# Understanding Pep

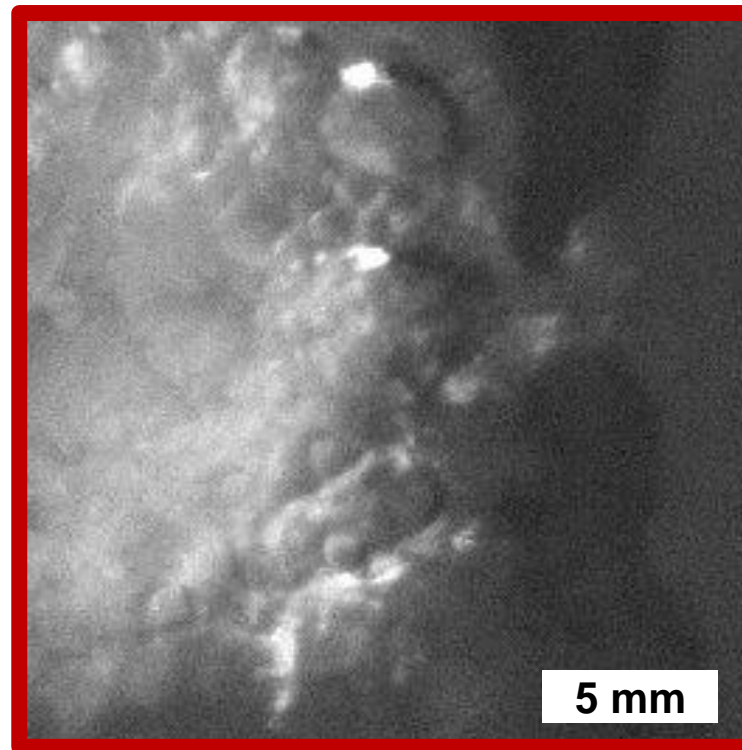
# Developement of VGE

High-speed Camera recordings starting submerged:  **$0.0 \text{ ms} \leq t \leq 8.33 \text{ ms}$**

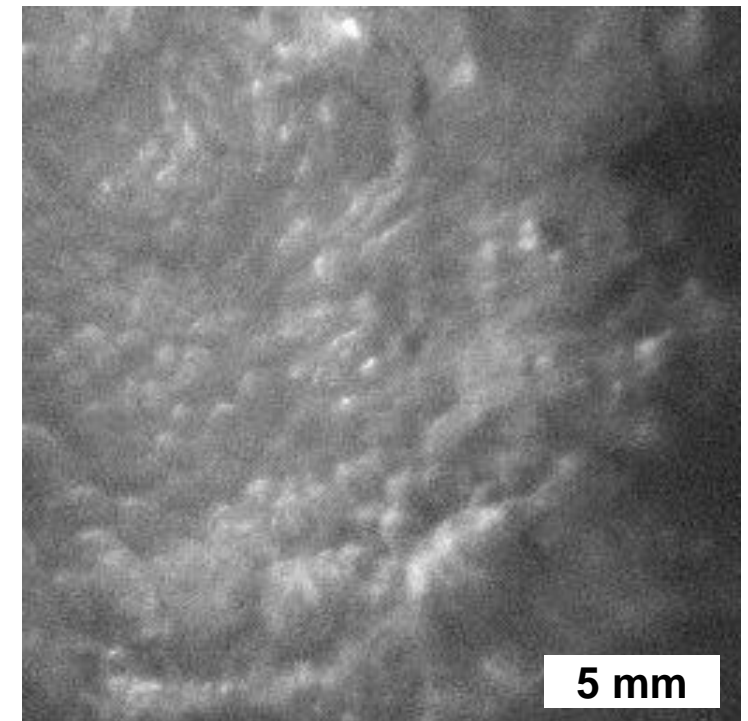
**$\rightarrow t = 4.17 \text{ ms}$**



316 V



340 V



360 V

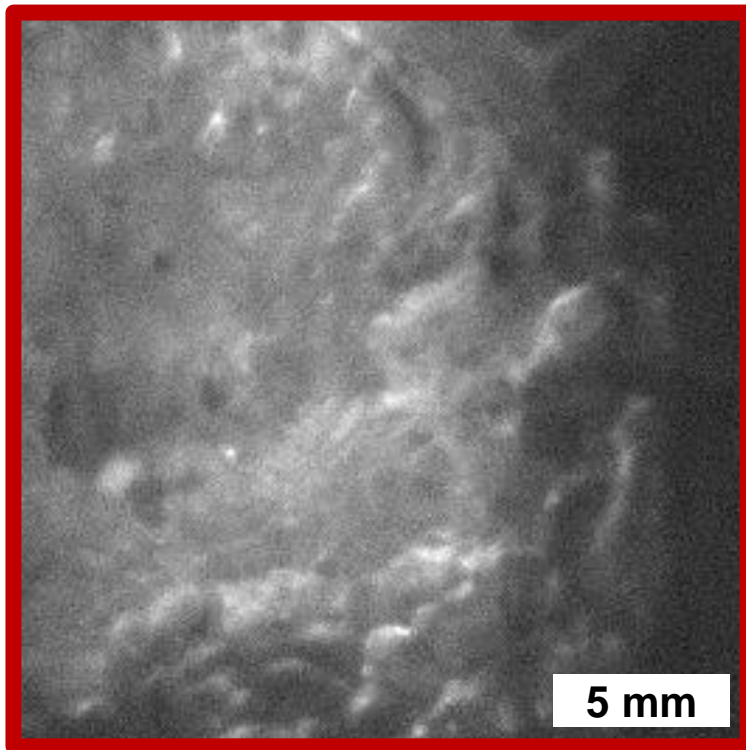
**$\rightarrow$  Very fast and high hydrodynamic process**

# Understanding Pep

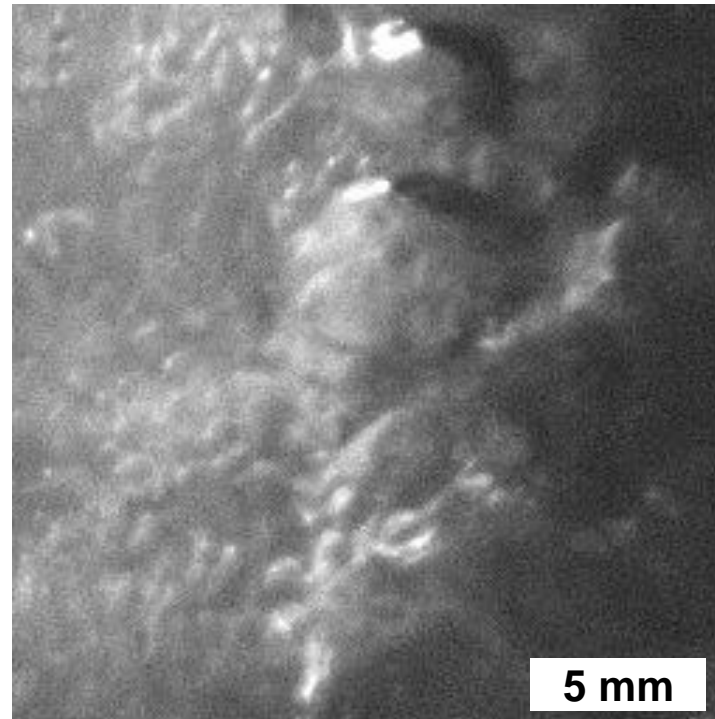
# Developement of VGE

High-speed Camera recordings starting submerged: **0.0 ms  $\leq$  t  $\leq$  8.33 ms**

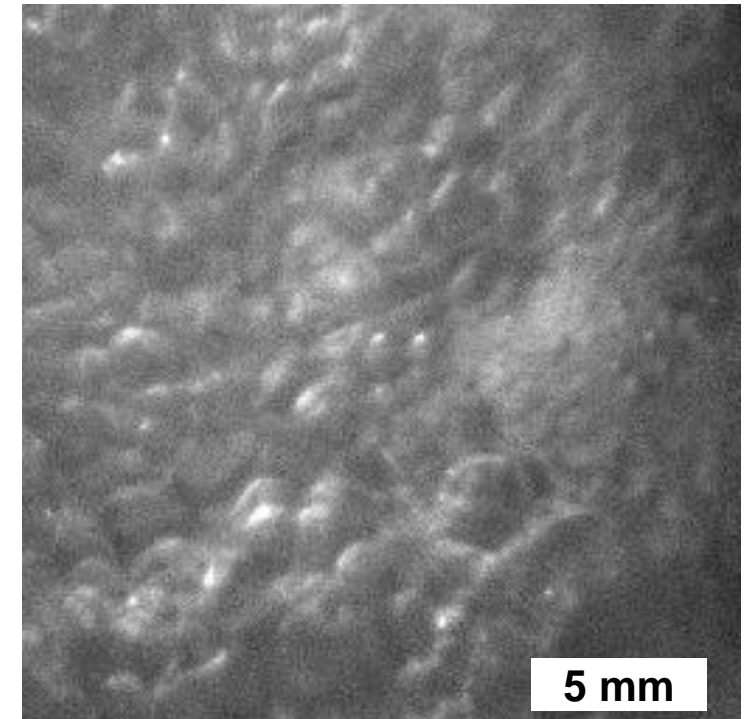
**$\rightarrow$  t = 5.00 ms**



316 V



340 V

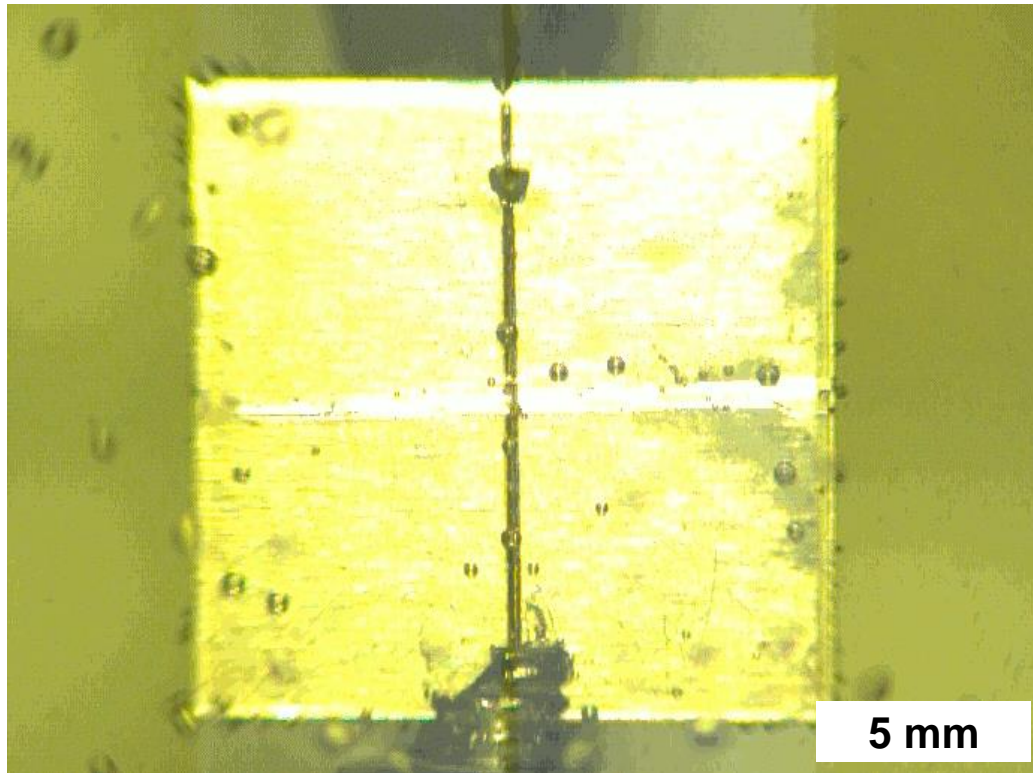


360 V

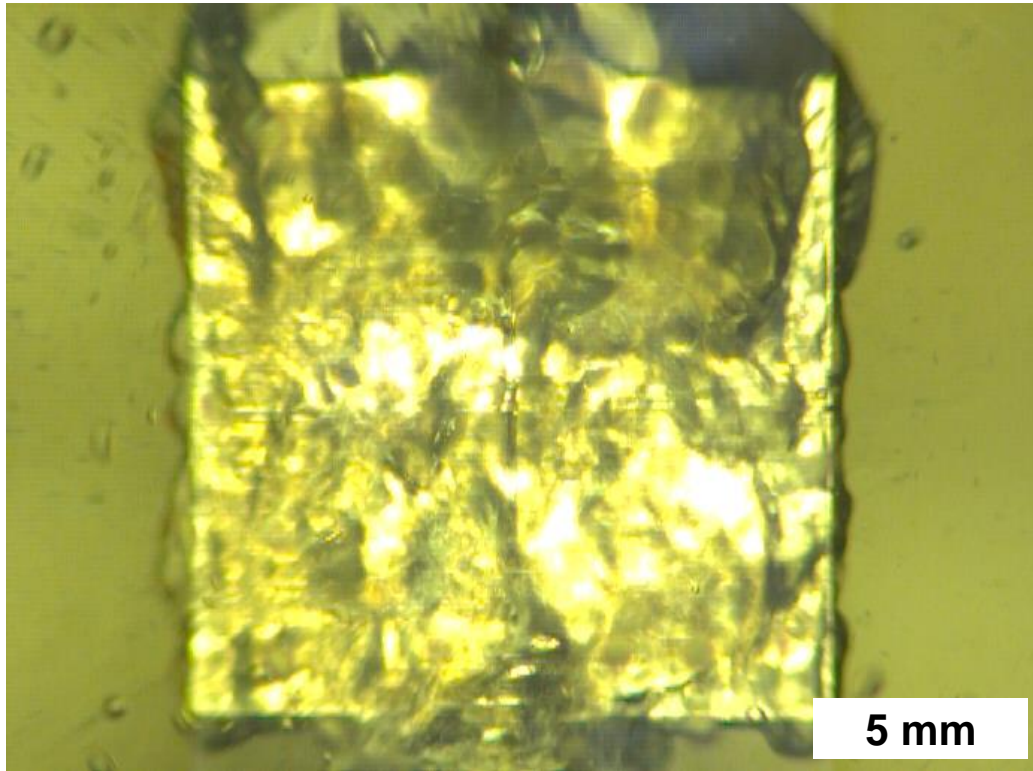
**$\rightarrow$  Very fast and high hydrodynamic process**

## Understanding Pep

stable process and continuous VGE



# Understanding Pep



## stable process and continuouse VGE

**continuouse:** → allover (vs. lokal breakdowns)

→ development

+

growing/merging

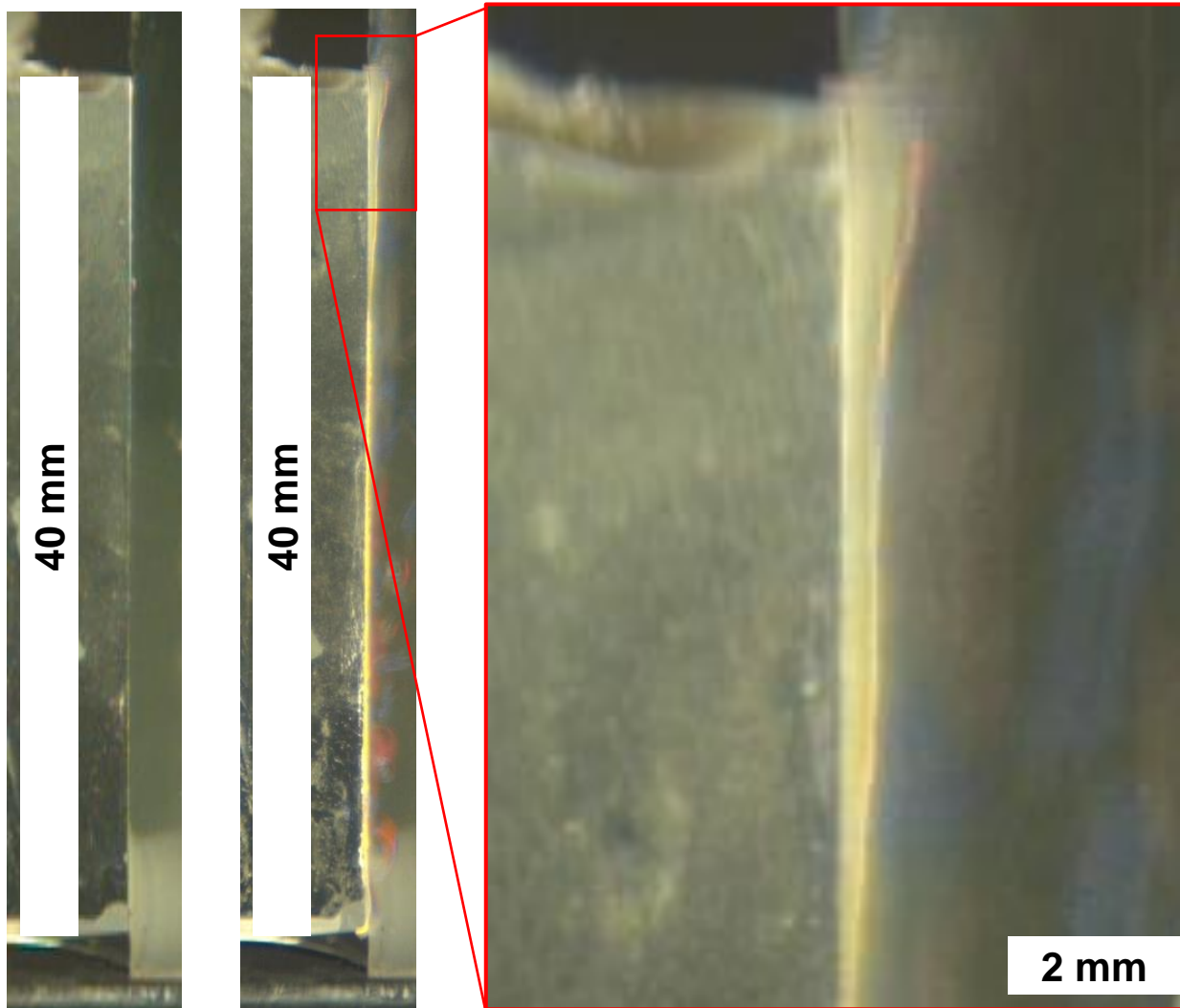
+

upraising and releasing from sample

... and

**pulsating:** → (lokal) thickness changes dynamically

## Understanding Pep



## VGE conditions over height

„cross section“ of VGE / plasma region:

→ sum up of vape/gas from bottom to top

→ (average) thickness grows from bottom to top



non-uniform conditions:

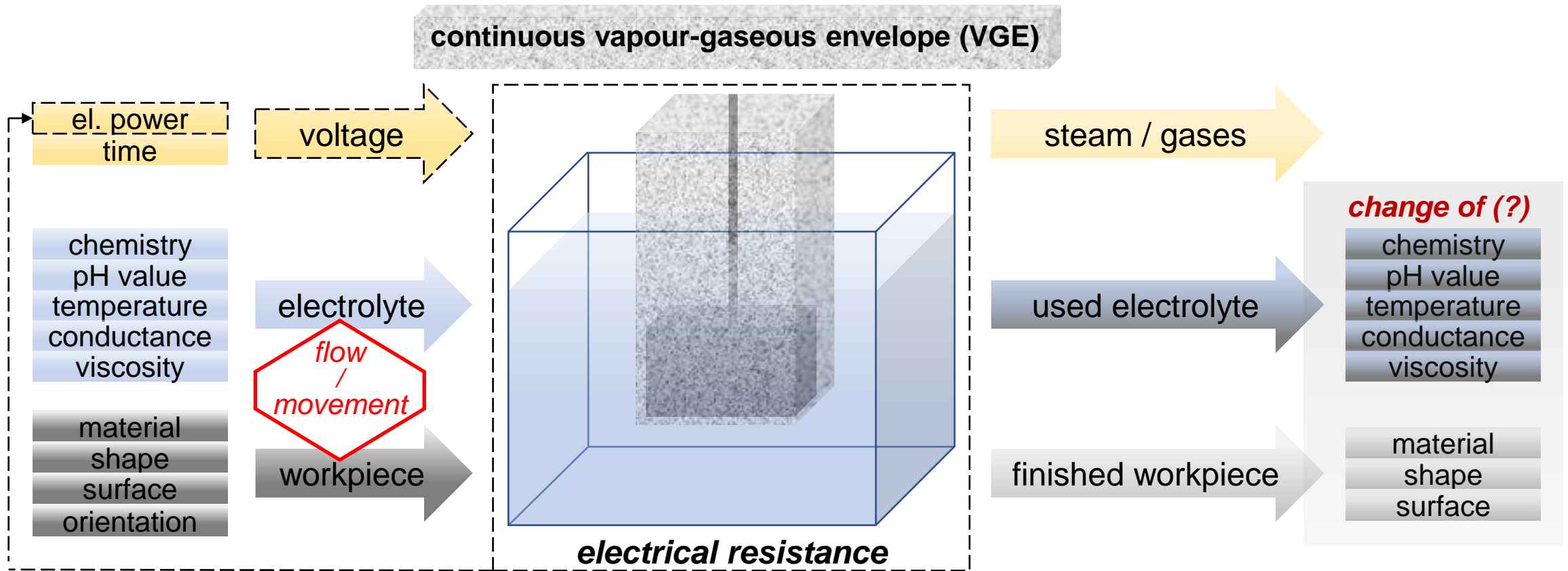
→ stronger material remove rate (MRR) and

→ higher gloss

down(side) than up(side)

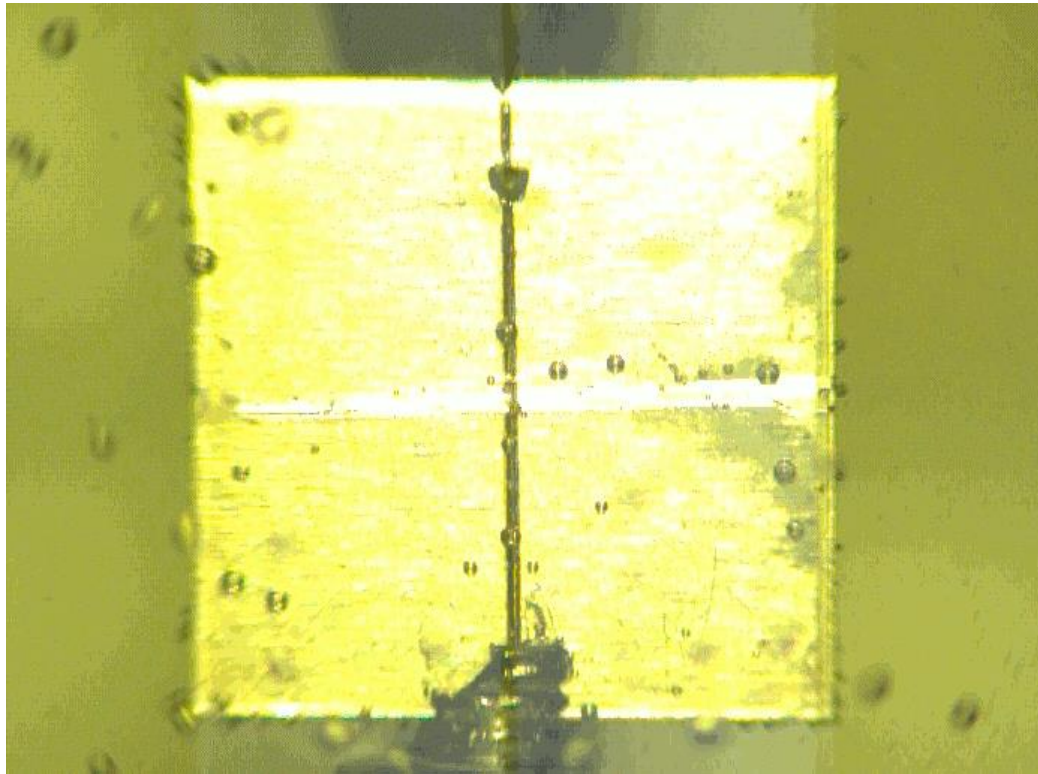
# Understanding Pep

## effect of electrolyt flow on VGE



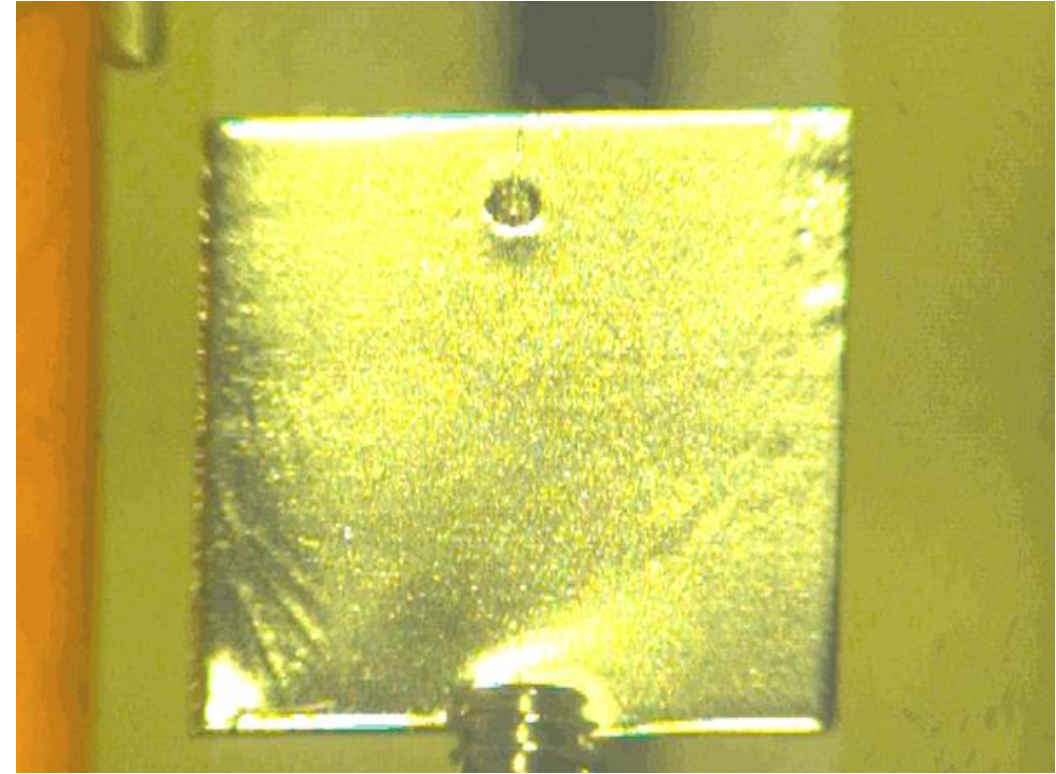
## Understanding Pep

no additional flow: 0 m/s



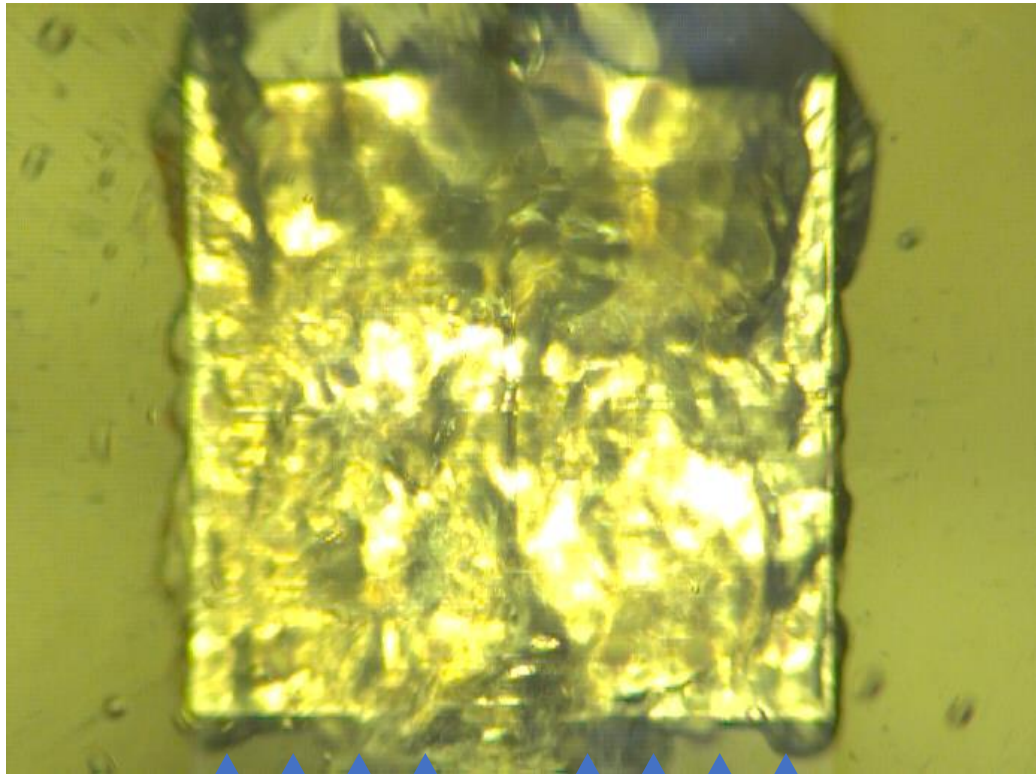
## effect of electrolyt flow on VGE

additional flow (from left): 1.2 m/s



# Understanding Pep

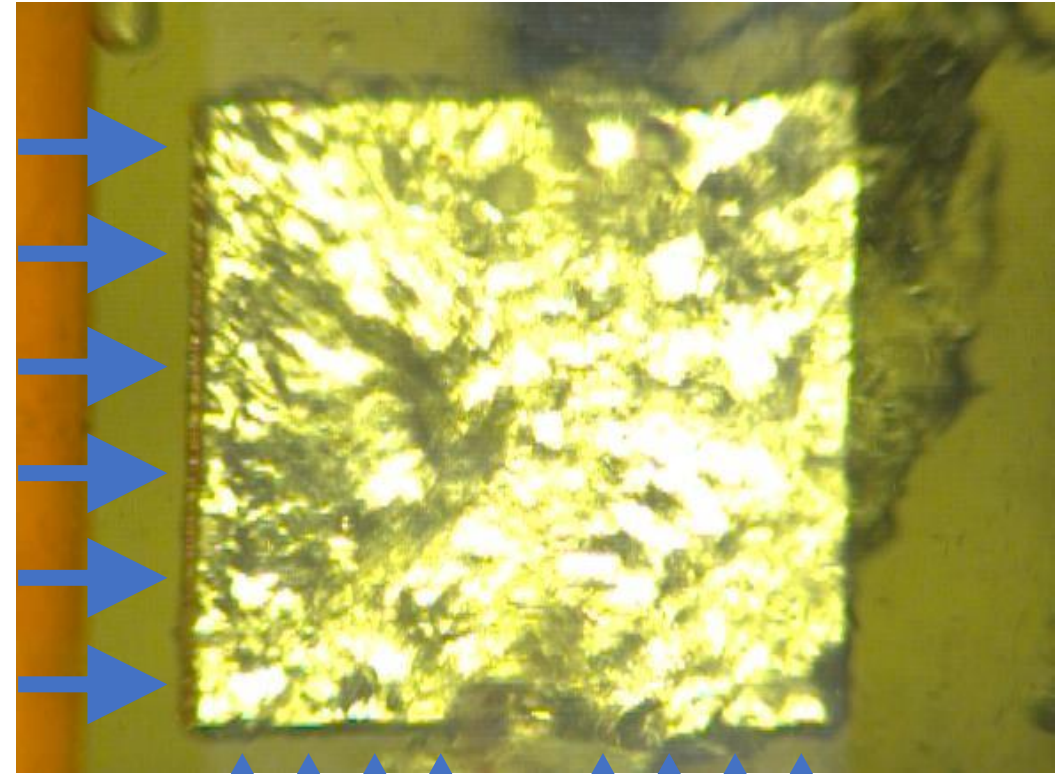
no additional flow: 0 m/s



“natural” electrolyte streaming

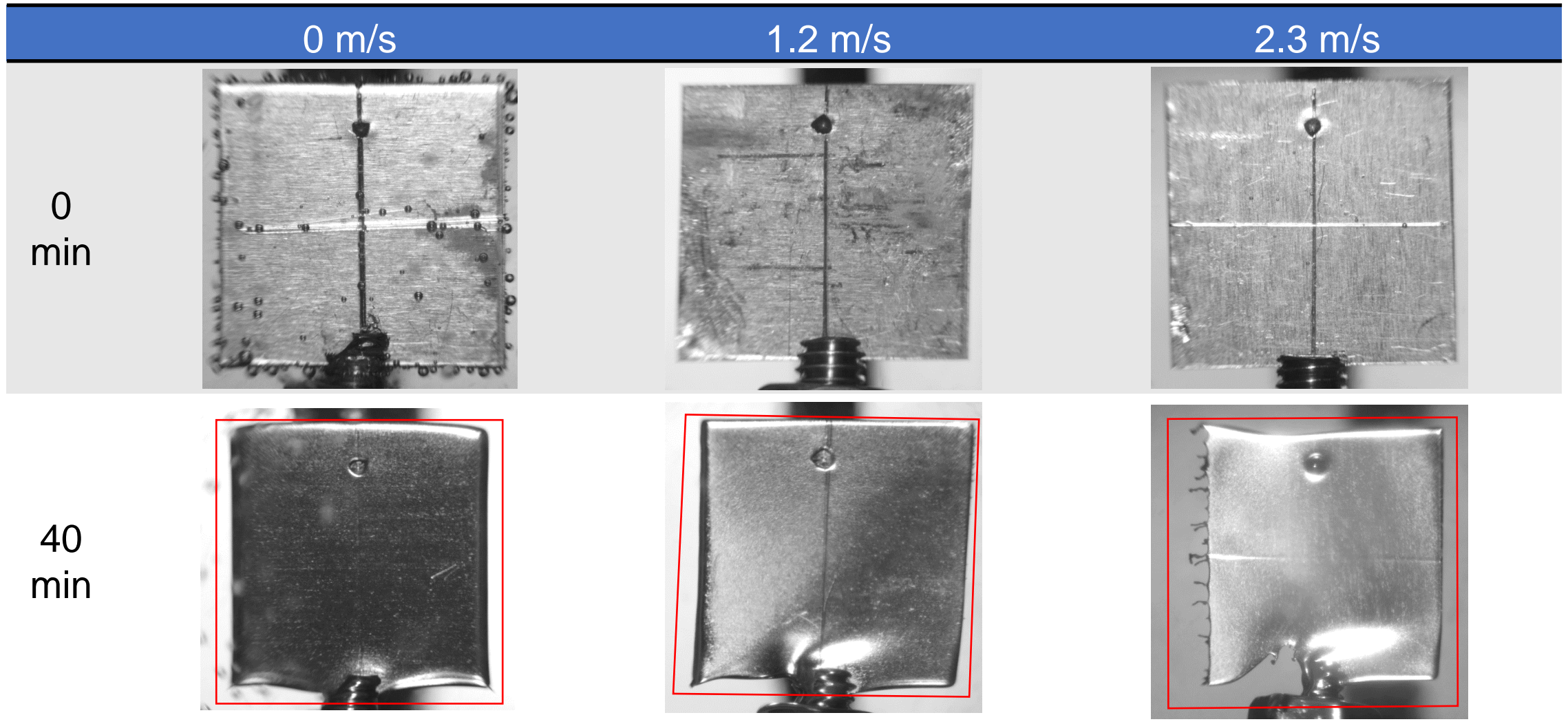
# effect of electrolyt flow on VGE

additional flow (from left): 1.2 m/s

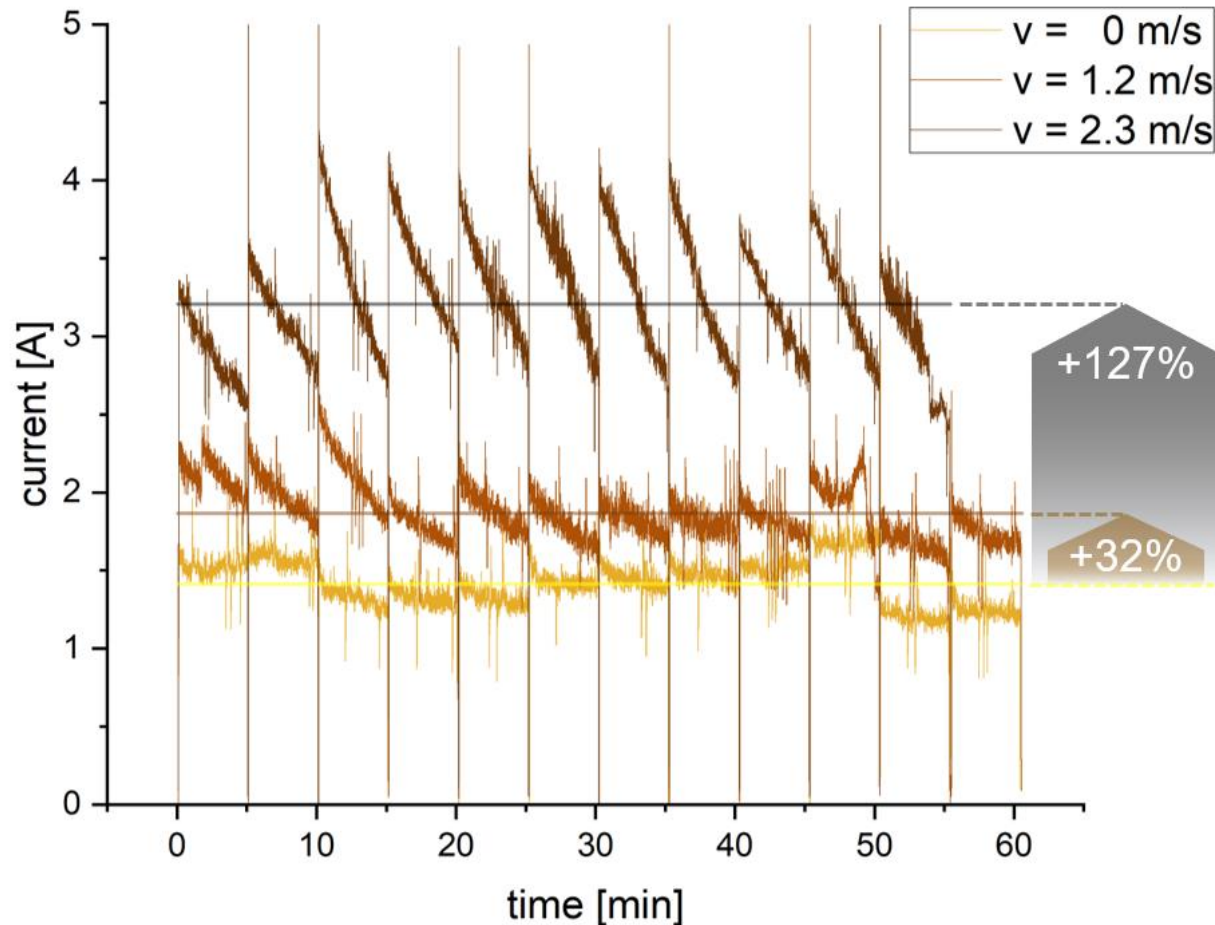


# Understanding Pep

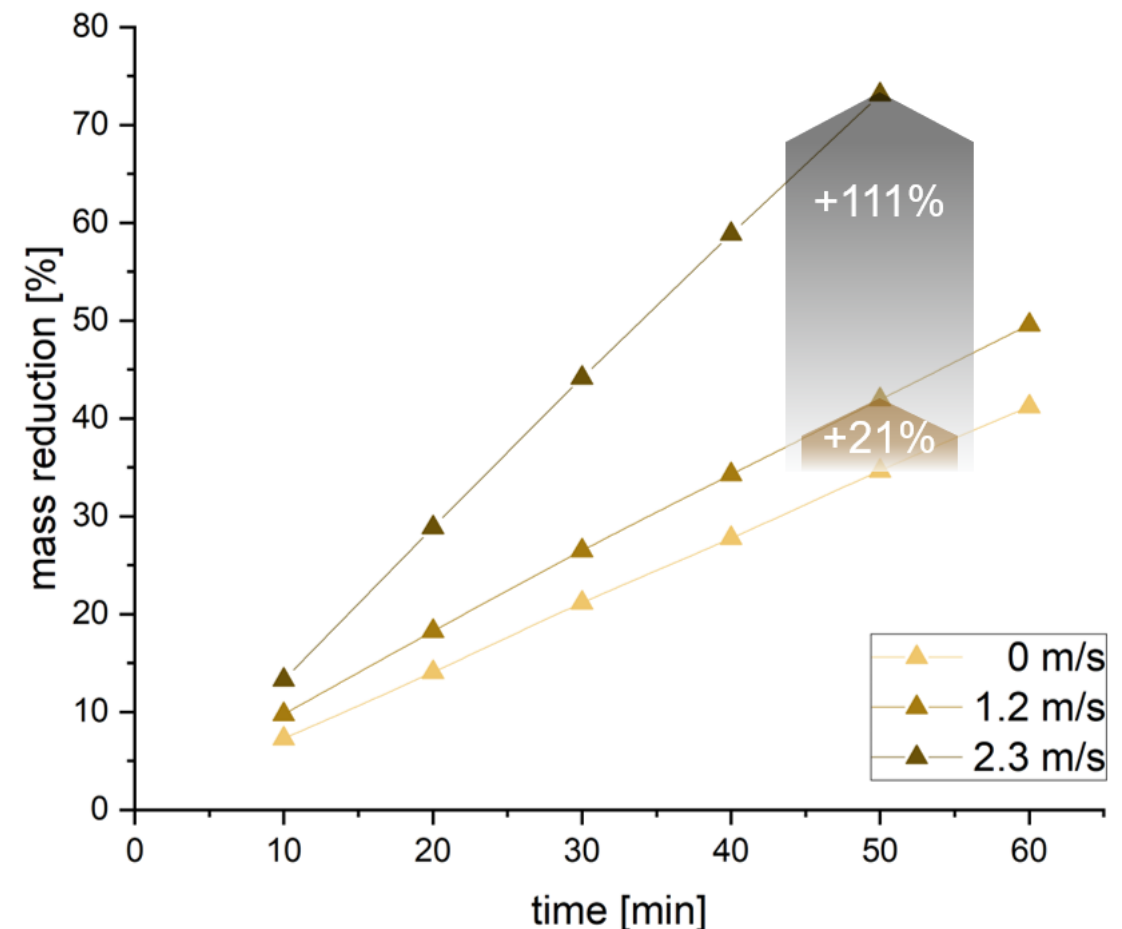
## effect of electrolyt flow on VGE



# Understanding Pep



# effect of electrolyte flow on VGE

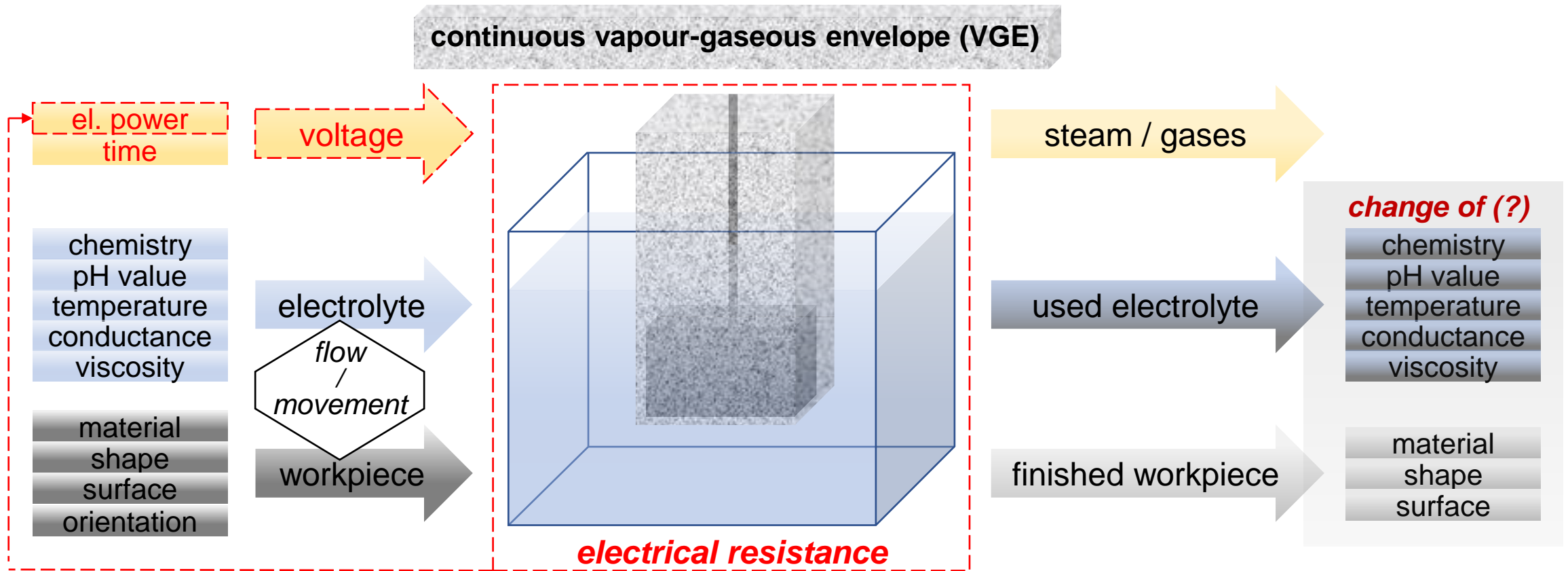


additional flow of electrolyte increase current density and material removal

**→ Relative movement surface – electrolyte: very strong effect on PeP-results!**

# Understanding Pep

energy



energy conservation law:

$$\begin{array}{lcl} E_{\text{input}} & = & E_{\text{output}} \\ E(\text{electrical} + \text{thermal} + \text{chemical}) & = & E(\text{electrical} + \text{thermal} + \text{chemical}) \end{array}$$

If the chemistry of the electrolyte has the opportunity to dissolve the workpiece material, a part of the input **electrical charge** will lead to the oxidation of the anodic workpiece (= material removal).

If not, it is mainly a **change of electric into thermal energy** (material removal and/or surface smoothing could be possible by local melting/evaporating of metal).

**electrical charges (current  $I$ ) = main drivers of PeP**

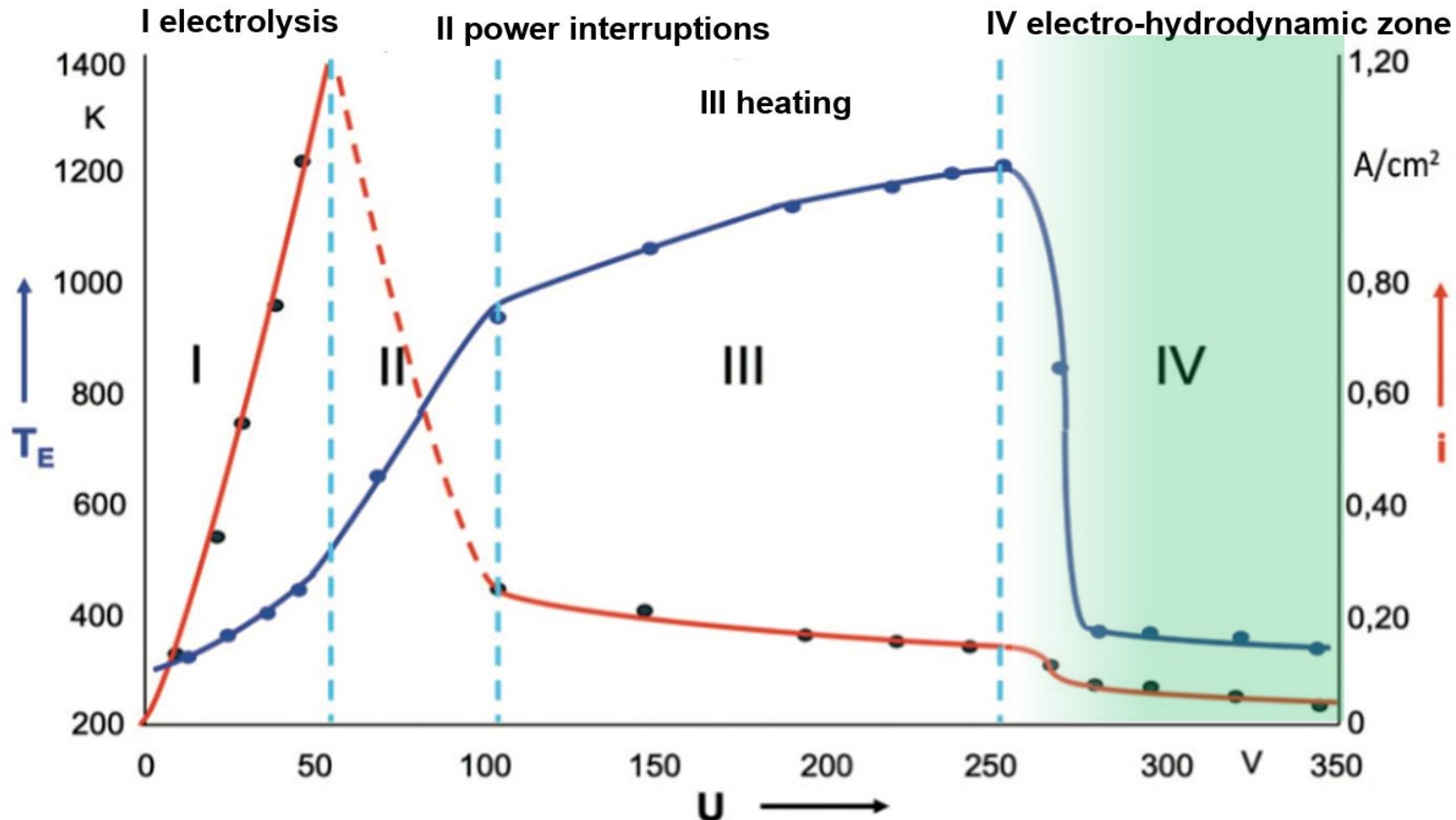
**+**

**voltage range ( $U = \sim 280$  to  $\sim 370$  V) for material removal AND high surface finish**

# Understanding Pep

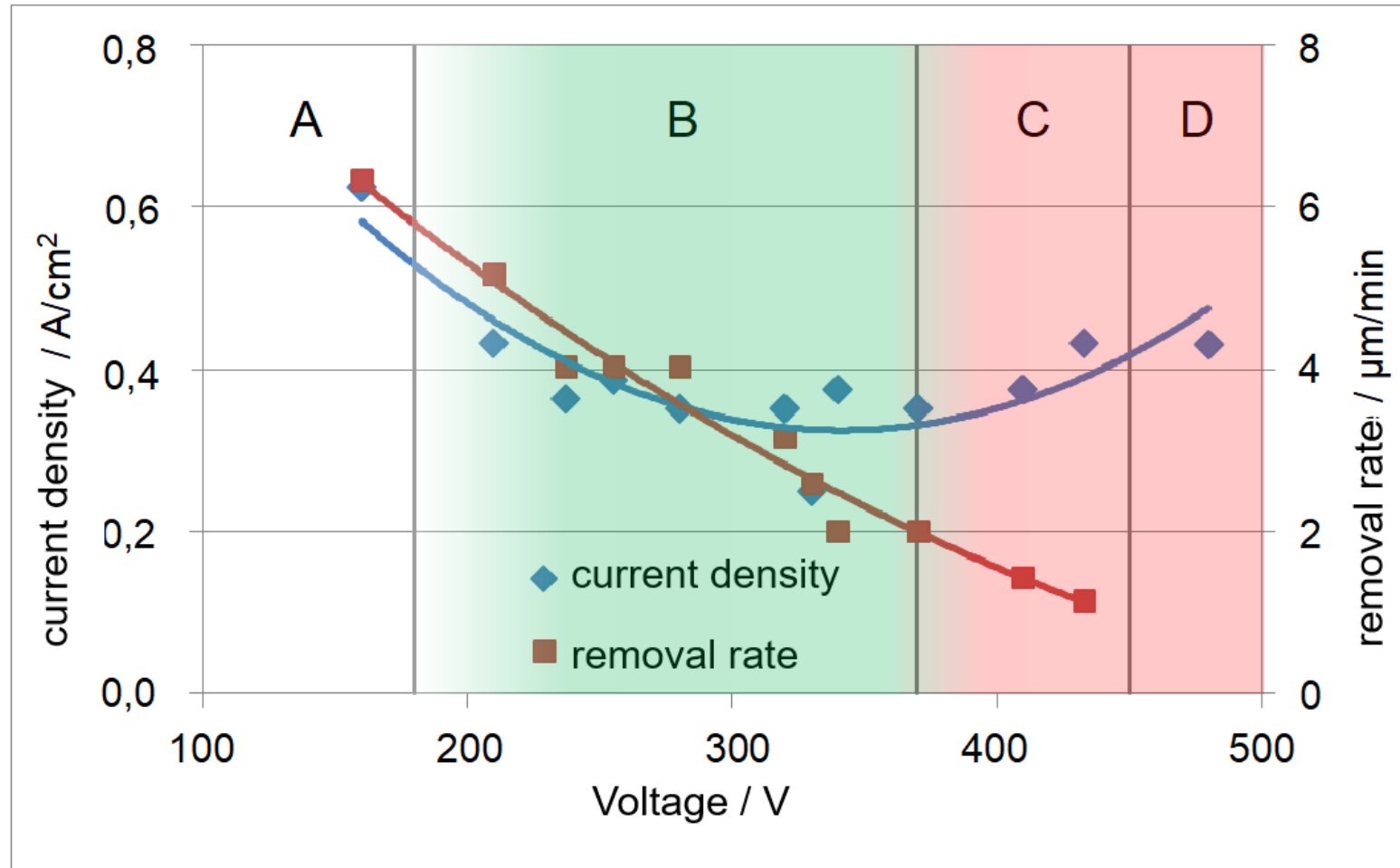
## lower voltage limit

**inside electro-hydrodynamic zone:** VGE leads to high thermal isolation ( $\rightarrow T_{\text{workpiece}} = \sim 100\text{ }^{\circ}\text{C}$ ) and electrical isolation (high voltage drop  $\rightarrow$  ionisation / plasma)



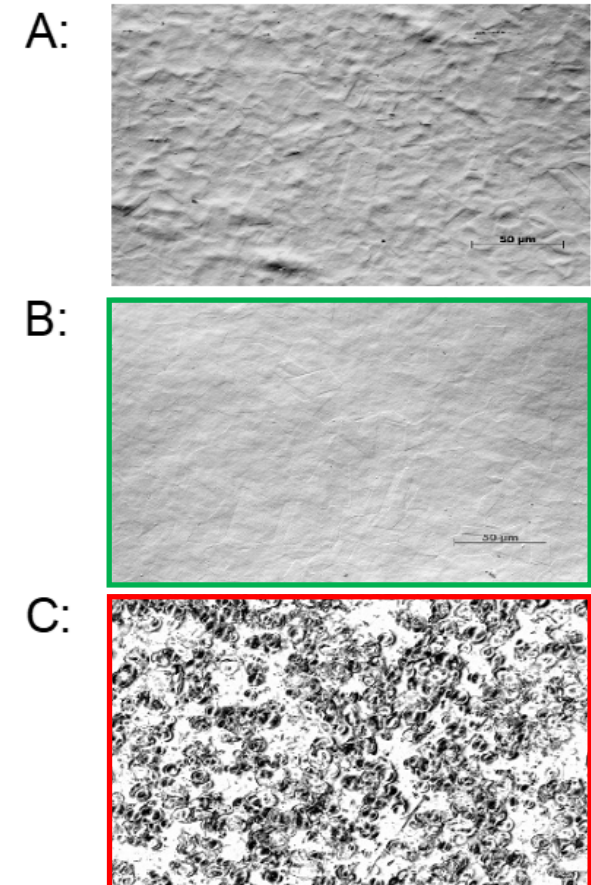
**voltage limit shifted** up or down, depending on resistance of system

# Understanding Pep



## upper voltage limit

surface topology



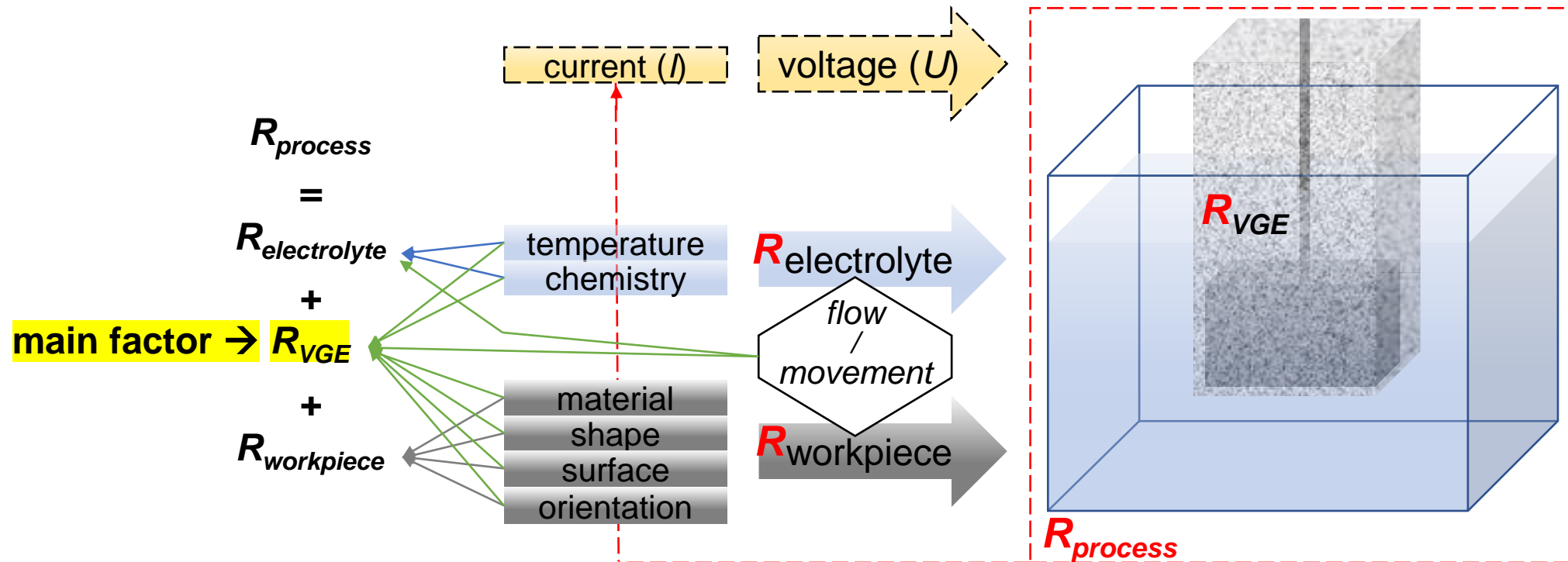
A – no stable plasma  
B – homogeneous plasma

C – glow- and spark discharge  
D – spark discharge

**Avoid! → craters**

# Understanding Pep

## electrical resistance and current



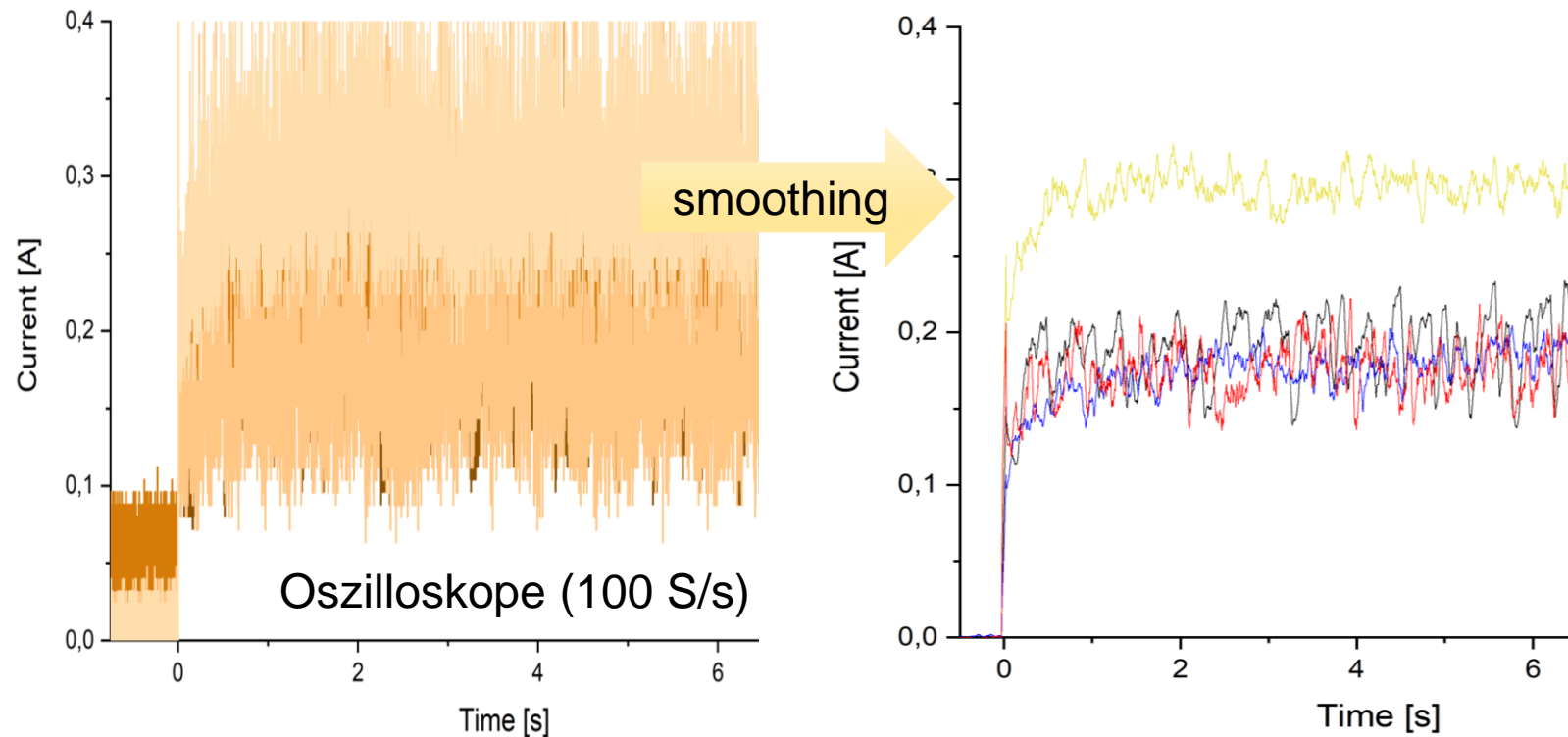
→ Ohm's law:  $I = U / R_{process}$

the resulting current(flow) is the main driver of the PeP-process  
(and also the main live-value/parameter to characterise the process)

→ Amount of charge  $Q(t) = \int I(t)dt$  most important/correct parameter on the input-side to describe  
"how much PeP" was done

# Understanding Pep

## measurement current/charge



**PeP is a highly dynamic process:  $10^3$  to  $10^x$ ? current jumps/second with large amplitudes**

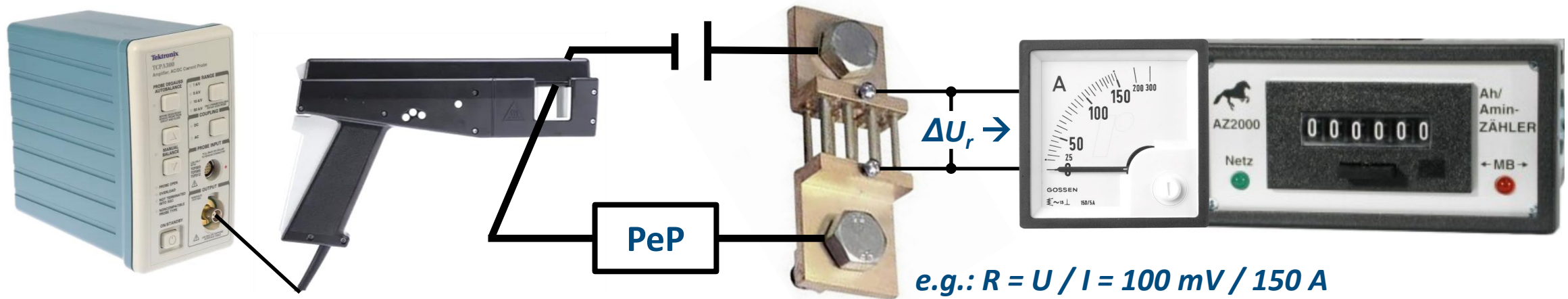
→ most exact measurement by oszilloskop, but: hard to read and lot of data → need of smoothing

→ digital displays: live values not good to read (fast changing)

→ physical needle analog meter (slugish behaviour = smoothing): good and simple to read

# Understanding Pep

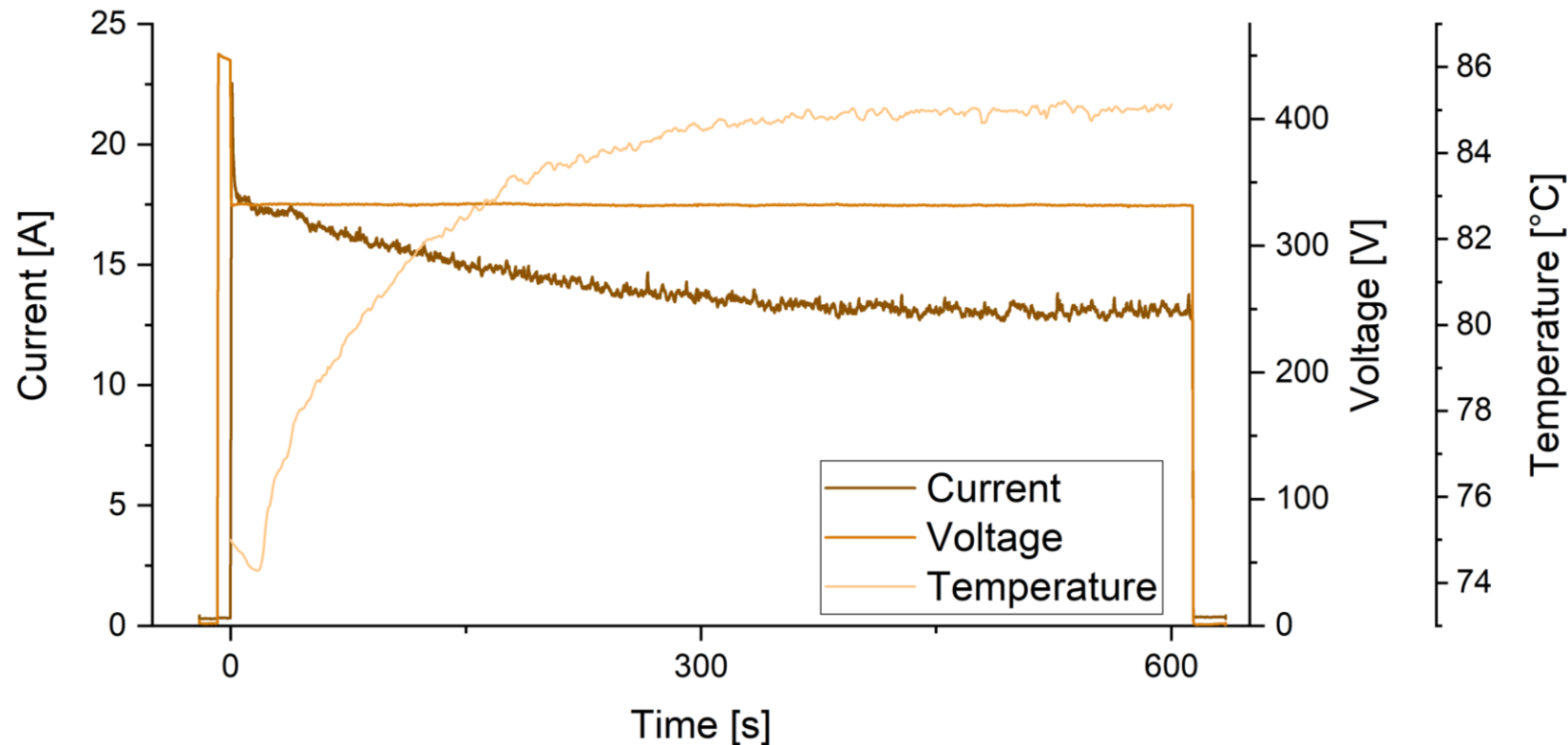
## measurement of current/ charge



	current probe + amplifier	shunt	charge integrator
principle	magnetic field of cable + Hall effect	voltage drop of a defined resistor ( $I = U / R$ )	voltage drop of <b>shunt</b> → integrating current over time
advantages	current circuit not affected contactless easy to use and safe	high accuracy (also current spikes) direct measurement cost-effective	easy to read cost-effective
dis-advantages	less accuracy at low current sensitiv to magnetic fields over range spices problematic expensive	circuit interruption → (small) voltage drop	

# Understanding Pep

## current and temperatur



- current spike due to fast immersion of the part and formation of VGE
- continuous drop of current due to increasing temperature and smoothing of surface and so decreasing the real surface area

$$I = U / R \text{ and } U \text{ is constant}$$

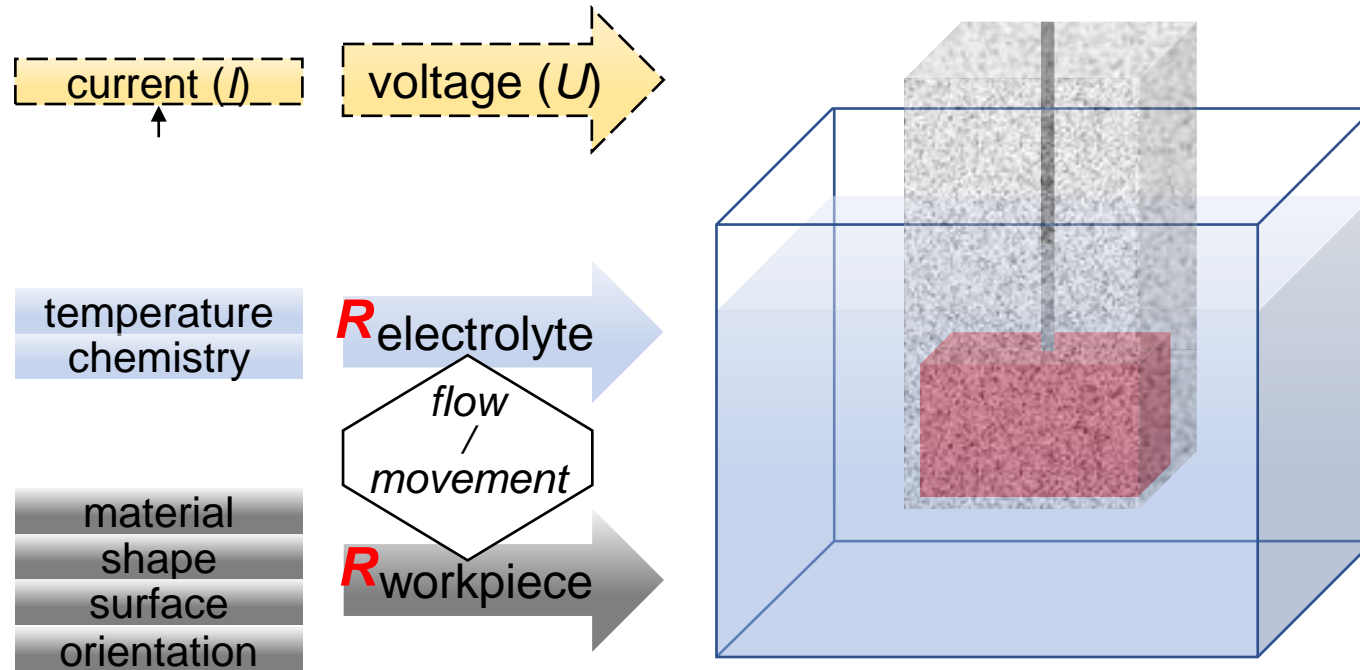
- when measured current is lower at higher temperatures then the (total) resistance must be higher
- higher temperatur of workpiece: → higher resistance
- higher temperature of electrolyte: → higher mobility of ions → lower resistance *but*  
→ thicker VGE (?) → higher resistance

$$I = U / R \text{ and } U \text{ is increased}$$

- current should be higher but there is no clear effect to see (compare to slide: upper voltage limit)
- higher voltage can influence chemical, physical and plasma processes so that the resistance is also increased and in total the current not increases

# Understanding Pep

current density



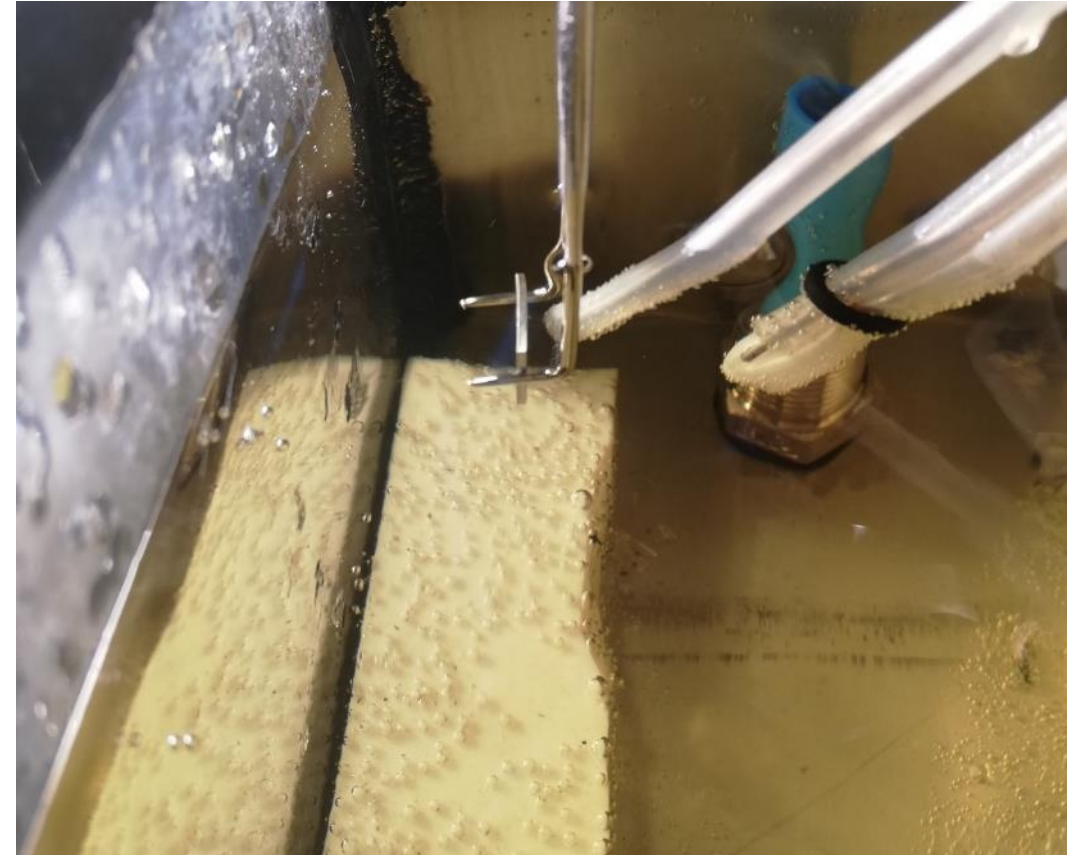
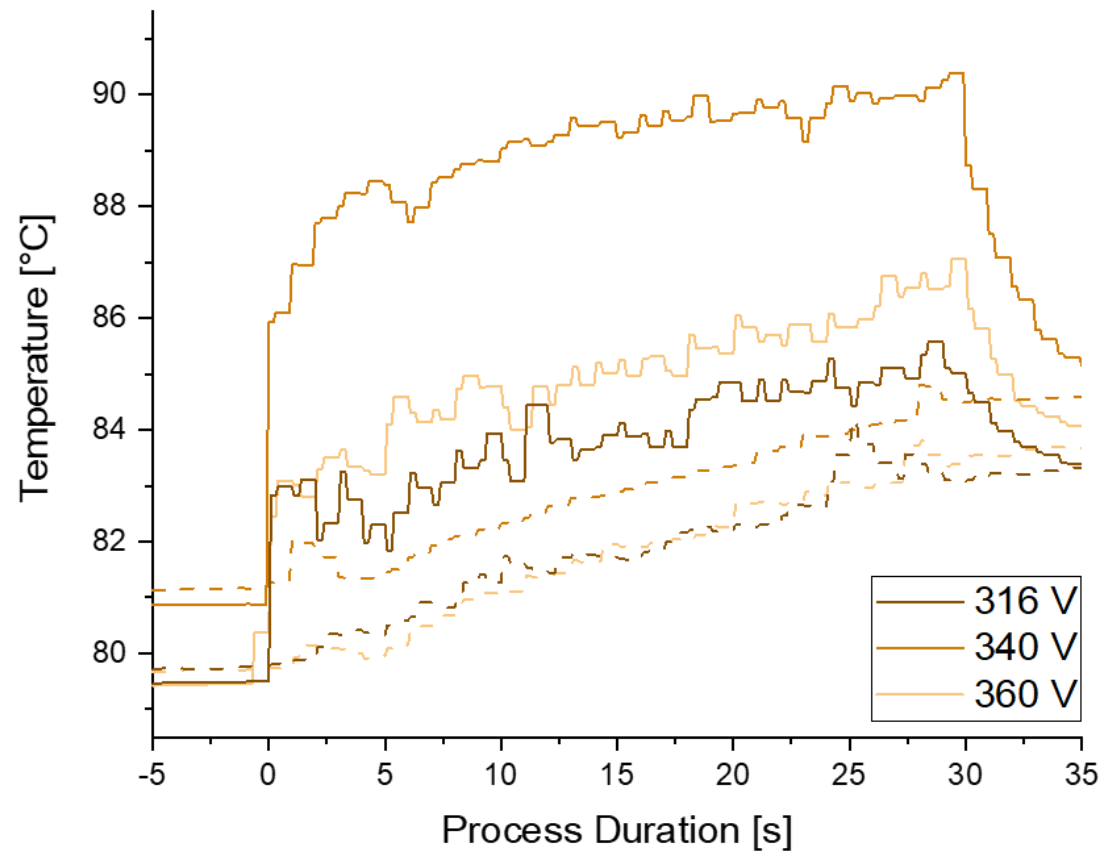
$\vec{J} = I / A_{\text{workpiece}}$  ... typically given in **A/cm<sup>2</sup>** is a value, that can describe how intensive the process works on the part

→ mainly affected by the conductivity (chemistry + temperature) of electrolyt and workpiece

→ typicall values: 0.1 – 0.4 A/cm<sup>2</sup>

# Understanding Pep

temperature



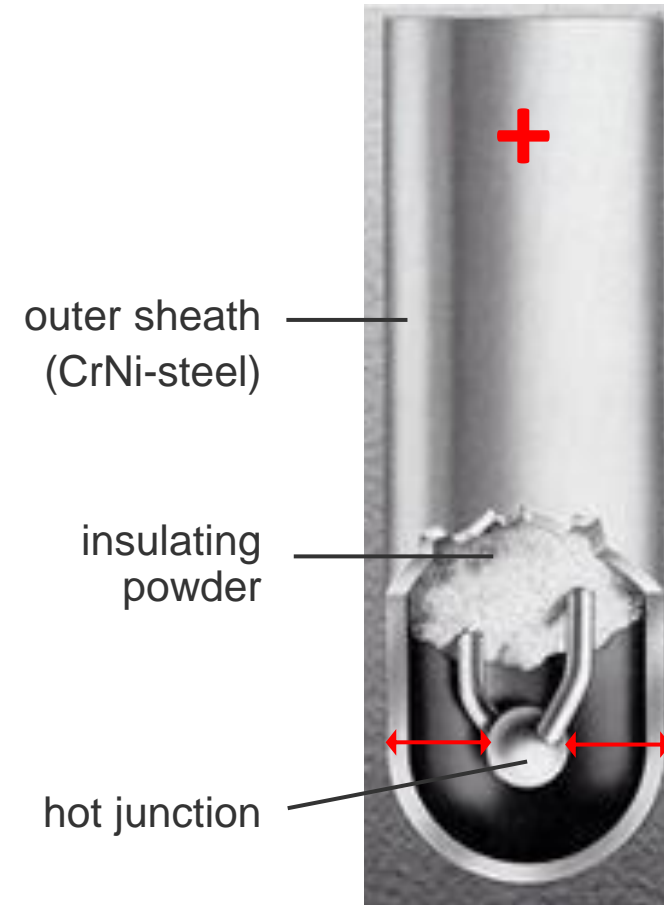
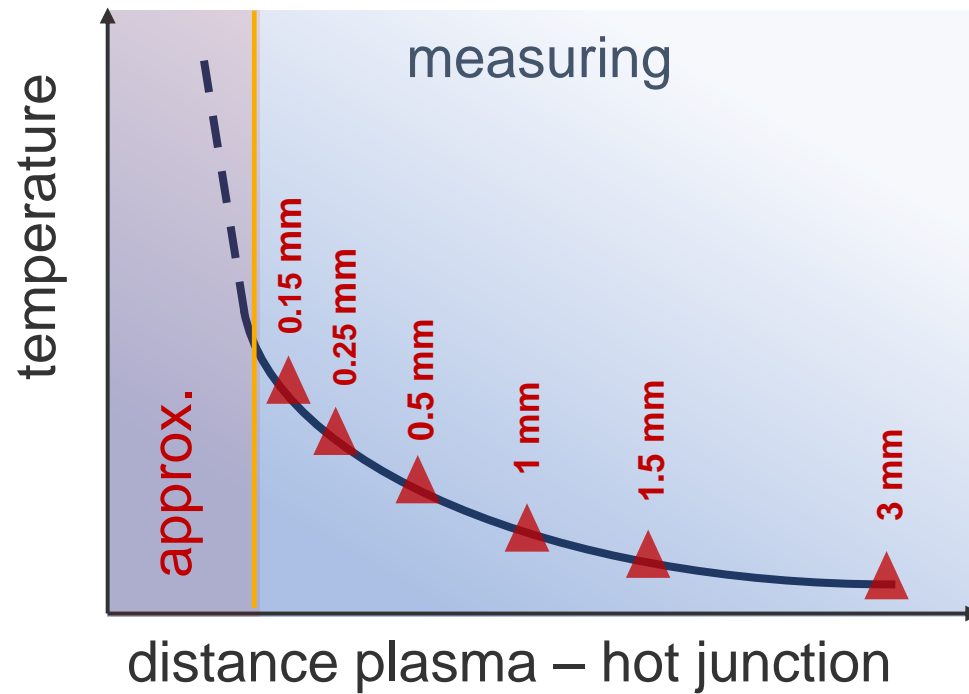
- electrolyte has not „one temperature“, it depends where it is measured

# Understanding Pep

temperature

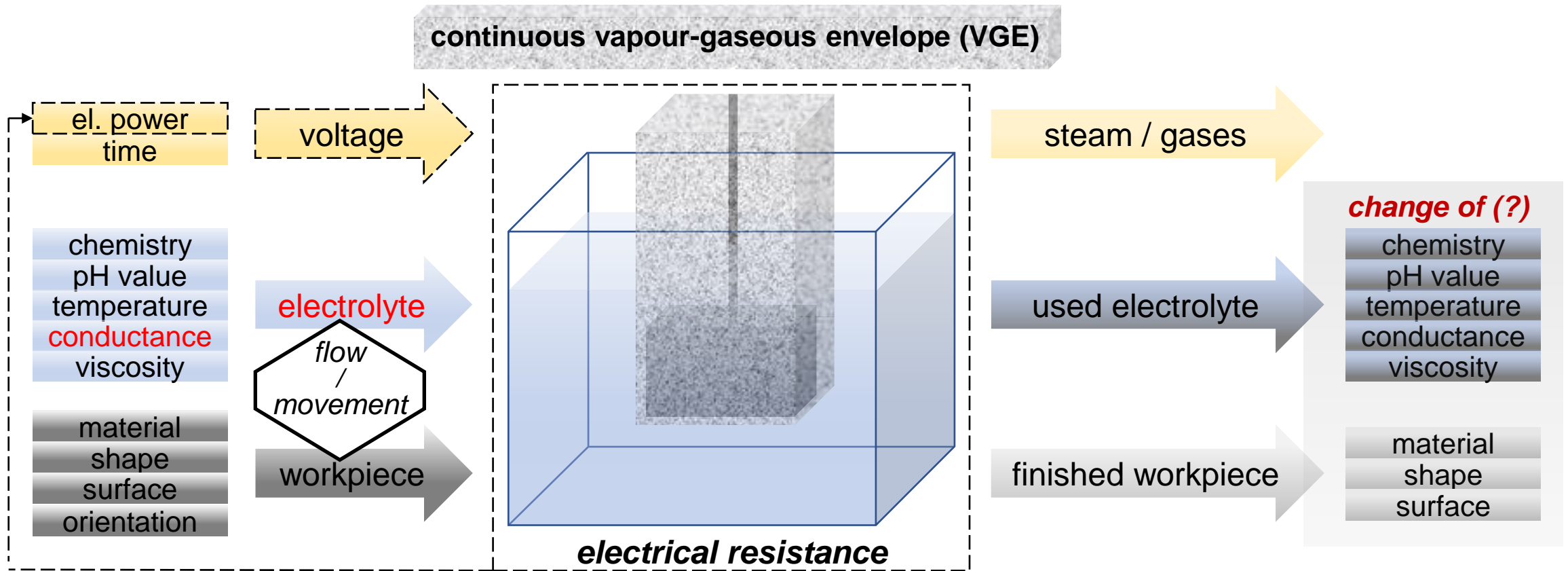
What's the temperature of plasma?

Can we measure it with thermocouple?



# Understanding Pep

## conductance of electrolyte solution



- conductivity ( $\kappa$ ) of electrolyte mainly influenced by the amount of solved salts/additives and it's temperature
- influences total resistance ( $R$ ) and thickness/stability of VGE:  $\rightarrow$  higher  $\kappa \rightarrow$  lower  $R$  of electrolyte and thinner VGE (also lower  $R$ )  $\rightarrow$  higher current  $\rightarrow$  *can* increase material removal, but also surface roughening



- conductivity meter with measurement cell with 2 or 4 electrodes
- AC voltage applied across electrodes → depending on resistant between electrodes a measuring current flows
- measured resistance is converted into conductivity in mS/cm (typical unit for PeP) by:  $\kappa = K/R$
- with the cell constant  $K = d / A$ , influenced by distance (d) and area (A) of the electrodes

**our target: conductance  $\kappa$  of 100 – 140 mS/cm @ starting temperature (mostly 75 – 80 °C)**

### material removal rate (MRR):

- mainly used to describe how fast PeP works (e.g. given in gramm per minute)
- influenced by a lot of factors:
  - part (material, geometry, size, surface (+area) and it's orientation (and or it's movement)
  - electrolyte (conductance, chemical reaktions, temperature, lifetime) and it's flow
  - process: voltage → current/amount of charge (time)

→ very specific value and difficult to compare if more than one condition is changed (and most are changing even during the process itself!)

sometimes better to find other specific rates:

- material removal per charge (gramm per ampere minute)
- material removal per area (gramm per cm<sup>2</sup>)
- change of dimensions per time (µm/min) / per charge (µm/Amin) / ...

**higher temperature:      lower MRR but higher material removal per charge**

**→ PeP is slower but more efficient**

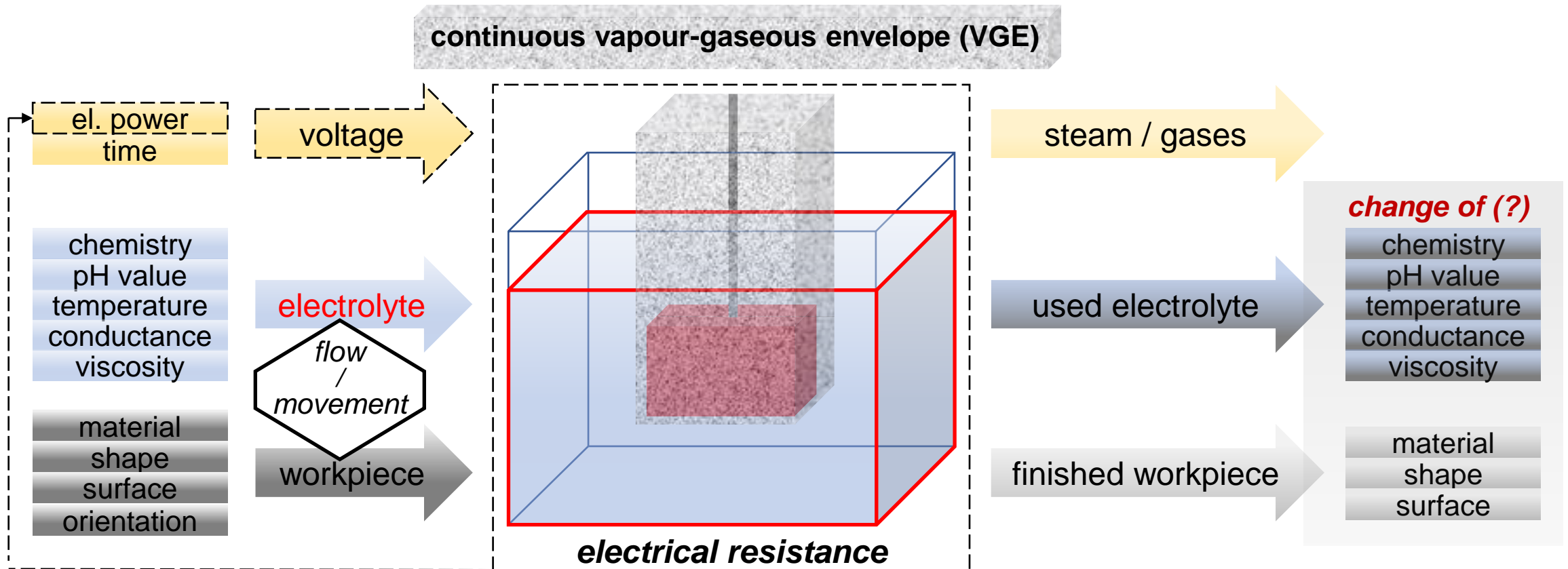
**higher temperature:      higher removal at spikes (burrs, edges,...) than on flat areas**

# UNDERSTANDING PEP

## Part 2: Electrolyte Solutions

# Understanding Pep

## electrochemical cell



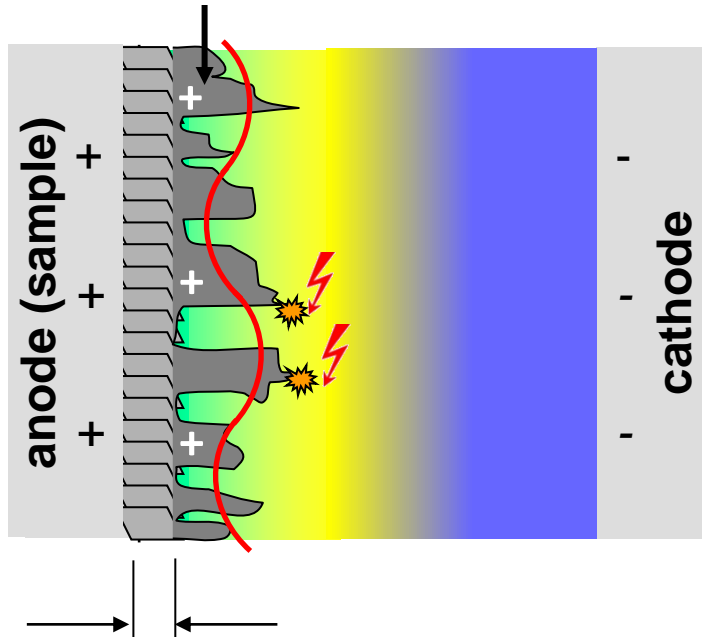
- chemistry of electrolyte solution is really important to achieve material removal, surface smoothing and gloss
- well working electrolyte composition has to be found for each single material/alloy

# Understanding Pep

# Material Removal Mechanisms

combination of electrochemical and physical processes

roughness  
(micro bumps)

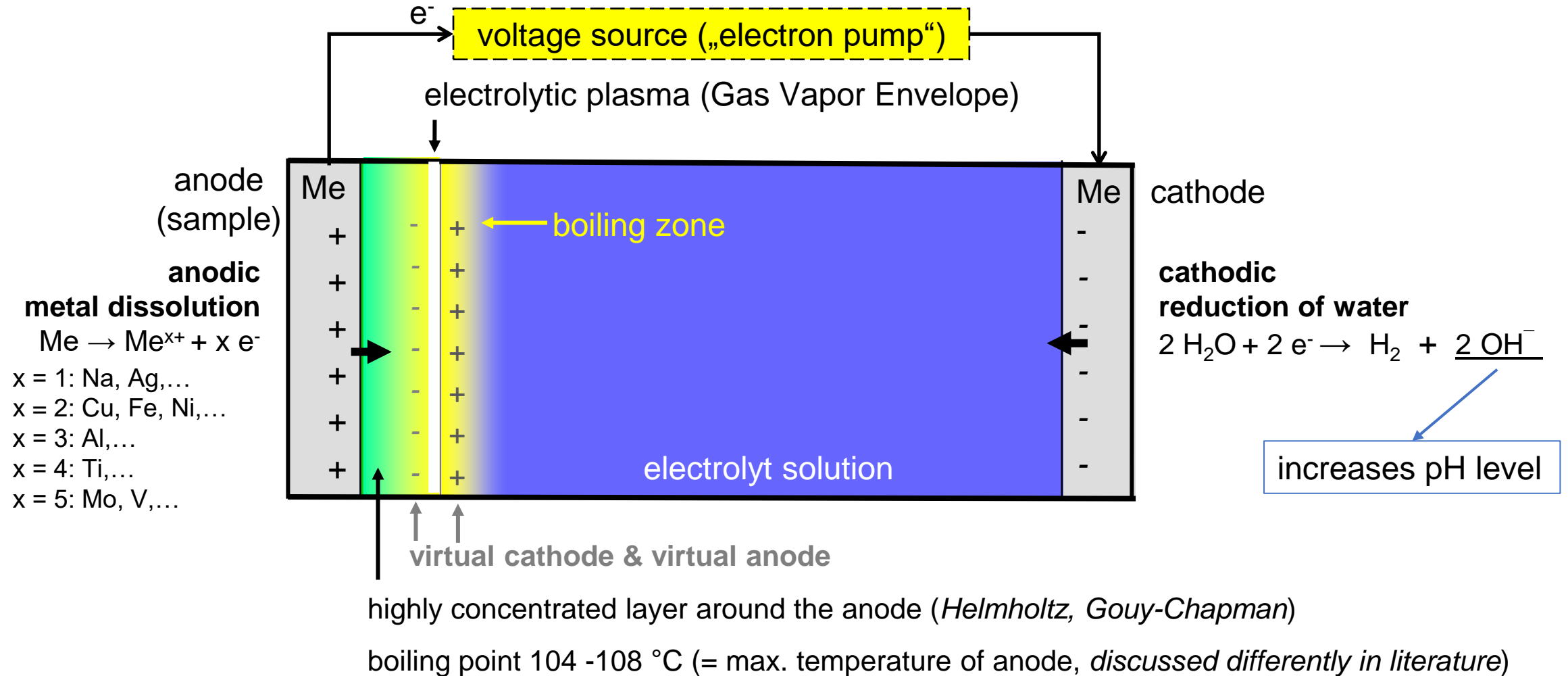


mechanism	
<b>electrolytic dissolution</b>	applied voltage → electric field forms → metal ions dissolve from surface into electrolyte
<b>plasma discharge</b>	high voltage → plasma region with high-energy ions, electrons, and neutral atoms (highly reactive) → enables material removal from surface by preferentially attacking microscopic peaks
<b>oxidation + chemical reactions</b>	plasma state and presence of oxygen → forming of less stable oxides on surface → easier to remove
<b>gas evolution</b>	gas bubbles + rising → remove of abraded material residues

Processing boundary layer (energetically activated area)

# Understanding Pep

## electrochemical cell/ reaction zones



Possible anode reactions under the conditions of PEP [80].

	Reactions	Potential (V) vs SHE	Reaction #
initial reactions at anode / cathode	$\text{Cr} + 2\text{H}_2\text{O} \rightarrow \text{Cr(OH)}_2 + 2\text{H}^+ + 2\text{e}^-$	-1.1	(7)
	$\text{Cr(OH)}_2 + \text{H}_2\text{O} \rightarrow \text{Cr(OH)}_3 + \text{H}^+ + \text{e}^-$	-0.6	(8)
	$\text{Fe} + \text{H}_2\text{O} \rightarrow \text{FeOH}^+ + \text{H}^+ + 2\text{e}^-$	-0.4	(9)
Further reactions with water and/or other ions in electrolyte	$\text{FeOH}^+ + \text{H}_2\text{O} \rightarrow \text{Fe(OH)}_2^+ + \text{H}^+ + \text{e}^-$	0.3	(10)
	$\text{Cr(OH)}_3 + \text{H}_2\text{O} \rightarrow \text{CrO}_4^{2-} + 5\text{H}^+ + 3\text{e}^-$	0.4	(11)
	$\text{Fe(OH)}_2^+ + 2\text{H}_2\text{O} \rightarrow \text{FeO}_4^{2-} + 6\text{H}^+ + 3\text{e}^-$	0.7	(12)
	$2\text{H}_2\text{O} \rightarrow 4\text{H}^+ + \text{O}_2 + 4\text{e}^-$	0.8	(13)
	$2\text{H}_2\text{O} \rightarrow \text{H}_2\text{O}_2 + 2\text{H}^+ + 2\text{e}^-$	1.8	(14)
	$2\text{SO}_4^{2-} \rightarrow \text{S}_2\text{O}_8^{2-} + 2\text{e}^-$	2.0	(15)



**formation of other ions or insoluble particles**

**main task: absorption + retention of metal ions in solution**

- water:
  - oxidation of Me
  - „produce“ VGE
- salts:
  - deliver ions as „charge carriers“ (mainly responsible for conductance)
- additives:
  - eg. acids, bases, complexing agents
  - in some cases: remove oxid layer (anodic) to start the process
  - keep anodic reaction products in solution (e.g. metal ions or oxides)
  - prohibit formation of metal oxides on the metal surface

Electrolyte solution needs to deliver a suitable medium (environment, e.g. pH-level) to enable material removal, surface smoothing and increase of gloss!

# Understanding Pep

## examples

### CrNi-steel @ acidic ammonium sulfate solution (sulfuric acid)

	Fe	Cr	Ni
Initial reaction (at anode)	$\text{Fe} \rightarrow \text{Fe}^+ + 2\text{e}^-$	$\text{Cr} \rightarrow \text{Cr}^{3+} + 3\text{e}^-$	$\text{Ni} \rightarrow \text{Ni}^{2+} + 2\text{e}^-$
Further reaction	$\text{FeOH}^+ + \text{H}_2\text{O} \rightarrow \text{Fe}(\text{OH})_2 + \text{e}^- \dots$	$\text{Cr}^{3+} + \text{SO}_4^{2-} / \text{NH}_4^+ \rightarrow$	$\text{Ni}^{2+} + \text{SO}_4^{2-} \rightarrow$
Further reaction products	$\dots \rightarrow (\text{NH}_4)\text{Fe}(\text{SO}_4)_2$ $\dots \rightarrow \text{Fe}(\text{OH})_3$	$\dots \rightarrow \text{Cr}_2(\text{SO}_4)_3$ $\dots \rightarrow (\text{NH}_4)\text{Cr}(\text{SO}_4)_2$	$\dots \rightarrow \text{NiSO}_4$
<b><u>Soluble (pH value)</u></b>	<b>&lt; ~ 3</b>	<b>&lt; ~ 5 and &gt; ~ 9</b>	<b>&gt; ~ 10</b>
↳ if not: precipitation of	insoluble red-brown depositions + mud	olive-green $\text{CrO}(\text{OH})$ -particles	light-green $\text{Ni}(\text{OH})_2$ -particles

- pH < ~1.8: chemical etching (also without voltage) → rough and matte surface!
- content of Fe > ~72 % → firmly adhering black oxid-layer ( $\text{FeO}$  and/or  $\text{Fe}_3\text{O}_4$ )

# Understanding Pep

## examples

### CrNi-steel @ sodium carbonate solution

	Fe	Cr	Ni
Initial reaction (at anode)	<b>nearly no reaction of Fe because oxidation of O<sub>2</sub> is energetically more favorable (2 OH<sup>-</sup> - 4e<sup>-</sup> → O<sub>2</sub> + H<sub>2</sub>O)</b>	<b>Cr → Cr<sup>3+</sup> + 3e<sup>-</sup></b>	Ni → Ni <sup>2+</sup> + 2e <sup>-</sup>
Further reaction		Cr <sup>3+</sup> + OH <sup>-</sup> → Cr(OH) <sub>3</sub>	Ni <sup>2+</sup> + CO <sub>3</sub> <sup>2-</sup> → NiCO <sub>3</sub>
Further reaction products		CrO <sub>4</sub> <sup>2-</sup> / 2 Na <sup>+</sup> + CrO <sub>4</sub> <sup>2-</sup> → Na <sub>2</sub> CrO <sub>4</sub>	
<b><u>Soluble (pH value)</u></b>		> ~ 9	good
↳ if not: precipitation of		yellow sediment	light green

very very low material removal when polishing CrNi-steel in sodium carbonate solution *but* high gloss

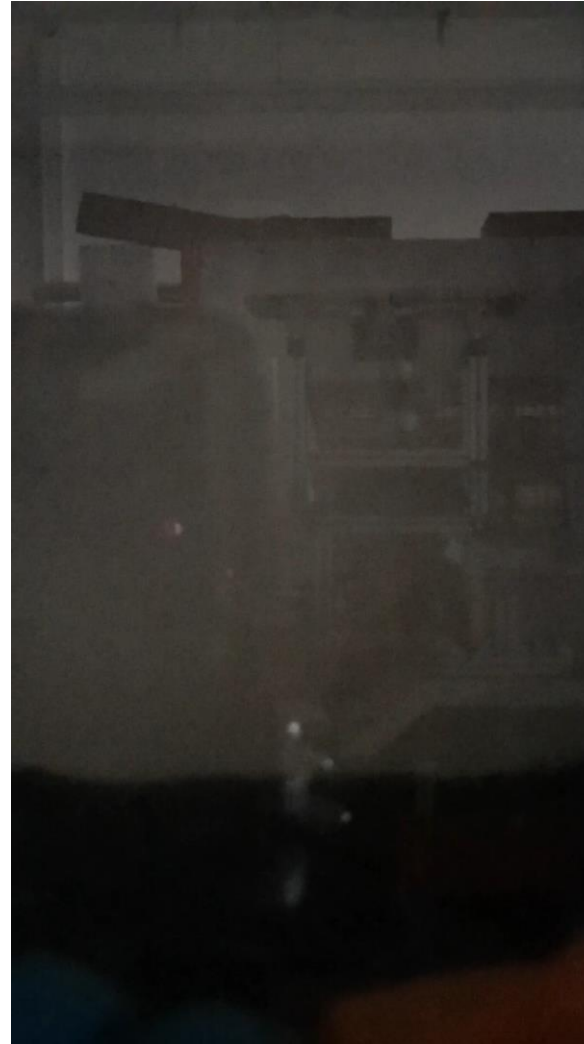
Caution!: Fe-rich surface → lower oxidation resistance

# Understanding Pep

examples

**CrNi-steel @ sodium carbonate solution**

typical: orange glowing of ionised sodium



### Copper @ acidic ammonium sulfate solution

→ development of copper sulfate layer ( $\text{CuSO}_4$ ) on anode

### Copper @ ammoniacal ammonium sulfate solution

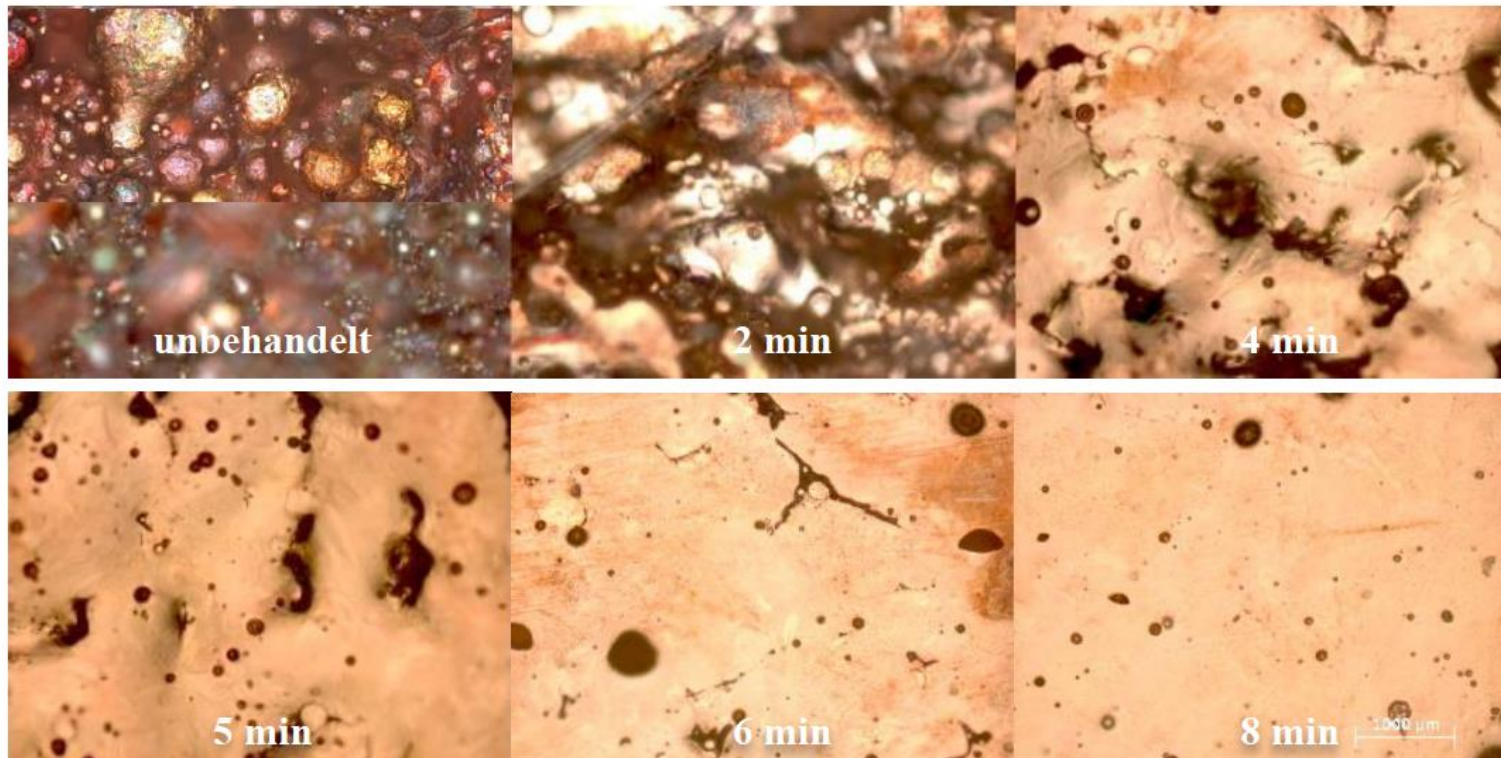
	Cu	
Initial reaction (at anode)	$\text{Cu} \rightarrow \text{Cu}^{2+} + 2\text{e}^-$	
Further reaction	$\text{Cu}^{2+} + 4\text{NH}_3 \rightarrow [\text{Cu}(\text{NH}_3)_4]^{2+}$	$\text{Cu}^{2+} + 2\text{OH}^- \rightarrow \text{Cu}(\text{OH})_2$
Further reaction products	$[\text{Cu}(\text{NH}_3)_4]^{2+} + 2\text{OH}^- \rightarrow \text{Cu}(\text{OH})_2 + 4\text{NH}_3$	$\text{CuO} \cdot \text{H}_2\text{O}$
<b>pH</b>	<b>8.1 – 8.7</b>	<b>&lt; ~ 9</b>
↳ if not: precipitation of	$\text{CuSO}_4$	unsoluble particles on anode

- ammonia ( $\text{NH}_3$ ) acts as complexing agent and stable  $[\text{Cu}(\text{NH}_3)_4]^{2+}$  is formed (Only between pH 8.1 – 8.7 and  $\text{NH}_3$  is present! If not: light blue depositons and/or no gloss)
- high material removal rates + good surface smoothing + high gloss achievable

# Understanding Pep

## examples

e.g.: Copper @ ammoniacal ammonium sulfate solution works well (see e.g. roughness)



t [min]	Ra	Rq	Rz
0	11,15		73,85
2	3,30	3,60	13,71
3	1,96	2,51	8,45
4	1,40	1,83	7,35
5	1,01	1,31	5,71
6	0,56	0,88	4,65
7	0,49	0,71	2,89
8	0,44	0,71	3,48

# Understanding Pep

## difficult materials and options

material	difficulties	options
low-alloy steel	rust and chemical etching	no strong acids → use citric acid
carbon-rich steel	graphit-coating of cathode	?
valve metals/alloys (Al, Ti, Zr)	hard-to-destroy oxide layers, matte surfaces	fluoric acid (!)
Si-rich alloys	matte grey surfaces, no gloss	?

- normally its enough to rinse with water
- high gloss surfaces tend to show water spots → deionised water and fast drying with pressurised air
- corrosion sensitive metals/alloy: well washing + rinse with ethanol + drying (oven), store dry and in protective atmosphere,(i.e. oil-bags or in ethanol), don't touch with bare hands
- rust from already corroded materials can be removed by PEP-treating them in citric acid-based electrolyte

**target: conductance  $\kappa$  of 100 – 140 mS/cm @ starting temperature (mostly 75 – 80 °C)**

→ salts (e.g. ammonium sulfate, ammonium chloride, sodium carbonate) = basic for conductance

approximation: aqueous solutions → increase of conductivity = ~ 2 – 3 % per K (range between 25 – 100 °C)

conductance  $\kappa$  depends on concentration  $c$  and molar conductance  $\lambda$  of ions ( $X^{n+}$  and  $X^{n-}$ ):

$$\kappa = c \cdot ( \lambda_{X^{n+}} \cdot [X^{n+}] + \lambda_{X^{n-}} \cdot [X^{n-}] )$$

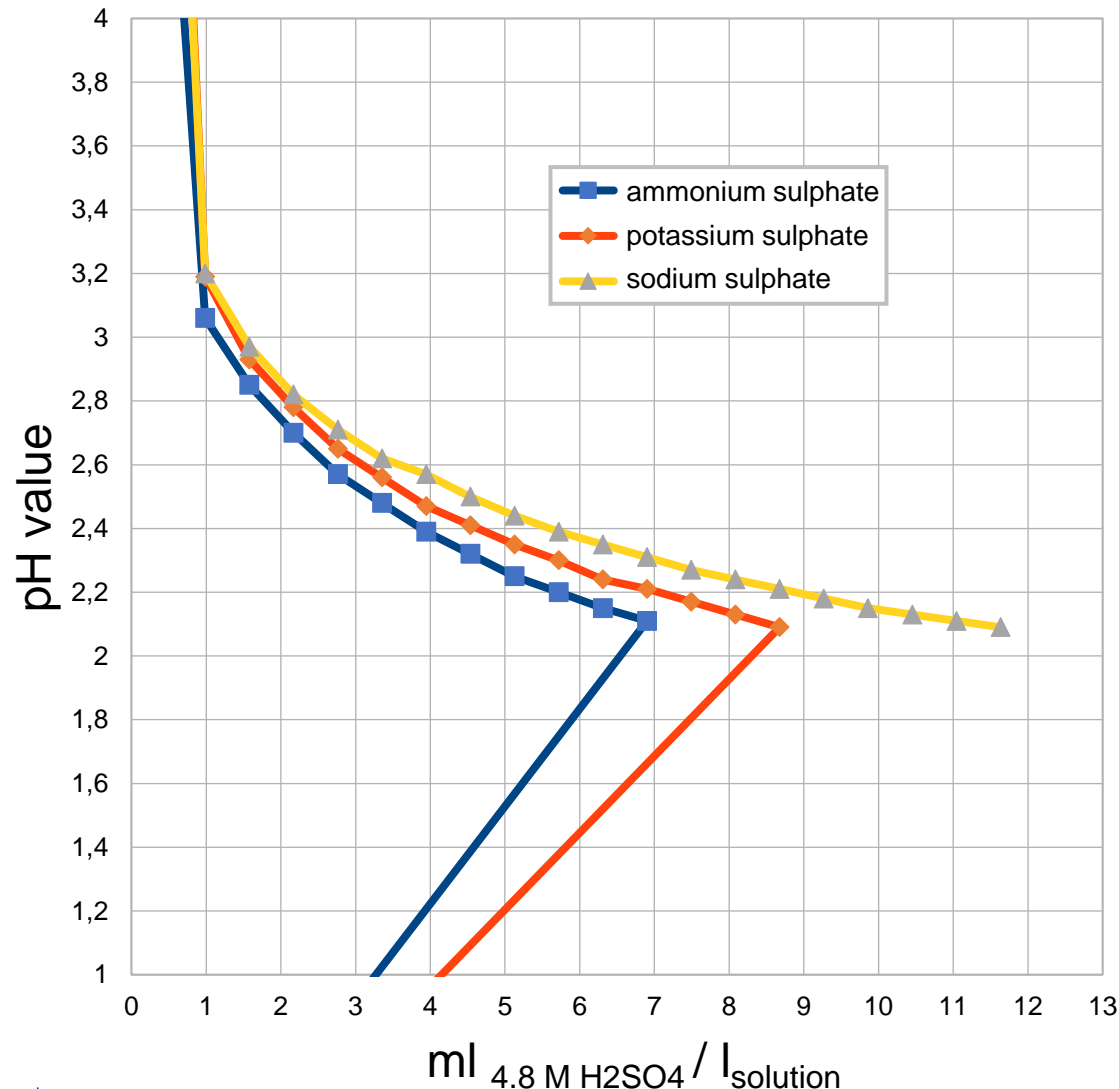
**target: suitable medium/environment (pH value) for required chemical reactions with anodic material**

→ use of: acids, bases, complexing agents,...

**other additives may influence conductance → take into account using the equation above!**

# Understanding Pep

# preparation of electrolyte solution



charts for resulting pH values (**measurements**) for different sulphatic solutions dependig on added 4.8 M sulphuric acid (ml/l)

4.8 M H<sub>2</sub>SO<sub>4</sub>  $\triangleq$  37% sulphuric acid solution  
→ reduced danger (e.g. “battery acid”)

→ easy to read and practical and for daily work

# Understanding Pep

# preparation of electrolyte solution

The regimes of steels PEP and the results obtained. Some data are rounded, in some cases, average values are indicated instead of the declared intervals.

Composition of aqueous solution (wt%)	Samples material	$U$ (V)	$T_{el}$ (°C)	$t$ (min)	$Ra$ (µm)	Ref.
4% ammonium sulphate and 0.25% hydrochloric acid	12Cr18Ni10Ti	270	35–40	5	0.02(0.20)	[109]
5% ammonium sulphate	20Cr13	250	70	15	0.06(0.45)	[55]
Sulphates of ammonia and sodium up to 30 g/l	AISI 201	250			0.06(0.24)	[61]
2% ammonium chloride	Low-carbon steel	300	85	15	0.09(0.63)	[106]
6% ammonium sulphate	20Cr13	300		15	0.13(0.53)	[106]
0.2 mol/l sodium sulphate	15CrMoV	320		10	0.14(0.39)	[111]
4% ammonium sulphate and 1% disodium ethylene diamine tetra acetate (Trilon B)	03Cr16Ni15Mo3	330	85–90		1.40(5.60)	[112]
0.24 mol/l ammonium chloride	30CrMnSi	311	–	8	0.17(0.93)	[107]
4–6% neutral salts	CrNi 18/10	–	65	5	0.78(1.70)	[59]
5% ammonium sulphate	20Cr13	300	70	15	0.06(0.32)	[99]
4% ammonium sulphate and 0.2% hydrochloric acid	08Cr18Ni10Ti	–	35–40	6	0.08(0.42)	[58]
0.2 mol/l ammonium sulphate	12Cr18Ni10Ti	380	85–90	3	0.65(1.80)	[126]
3% ammonium chloride and 1% ammonium sulphate, 0.5% Trilon B	38Cr2Ni2Mo	270	90	5	0.40(1.60)	[66]
8% ammonium sulphate	CrNi45MoWTiAlNbB	300	80	–	0.15(0.80)	[84]
5% ammonium sulphate	08Cr18Ni10Ti	270	85–90	5	0.17(0.63)	[117]
3% ammonium sulphate	SUS304	280	17	35	0.06(0.40)	[118]
18% sodium hydrocarbonate	12Cr18Ni10Ti	260	85		0.06(0.64)	[67]
5% ammonium sulphate and 0.8% Trilon B	CrNi45MoWTiAlNbB	300	73	2	0.18(0.60)	[120]
5–7% ammonium sulphate	12Cr18Ni10Ti	295	85–90	8	0.16(0.63)	[122]
3.4% ammonium sulphate	20Cr13	300	50–65	–	0.02(0.12)	[149]

**ammonium sulphate is often used because it (nearly) not take place in reaktionen → no loss of it**

Calculation for amount of acid to be added to water / pH value

*example of a acidic 0.33 M ammonium sulfate solution (sulphuric acid)*

Henderson-Hasselbalch equation:  $\text{pH} = \text{p}K_a + \log (c(\text{A}^-) / c(\text{HA}))$

pH... acidity of the solution

$\text{p}K_a$ ... **negative base-10 logarithm of the acid dissociation constant  $K_a$**  (acid dissociation constant at equilibrium state) *(1.99 for  $\text{H}_2\text{SO}_4$  at equilibrium of hydrogen sulfat/sulfat)*

$c(\text{A}^-)$ ... concentration of the conjugate base / negative ion ( $\text{SO}_4^{2-}$ )

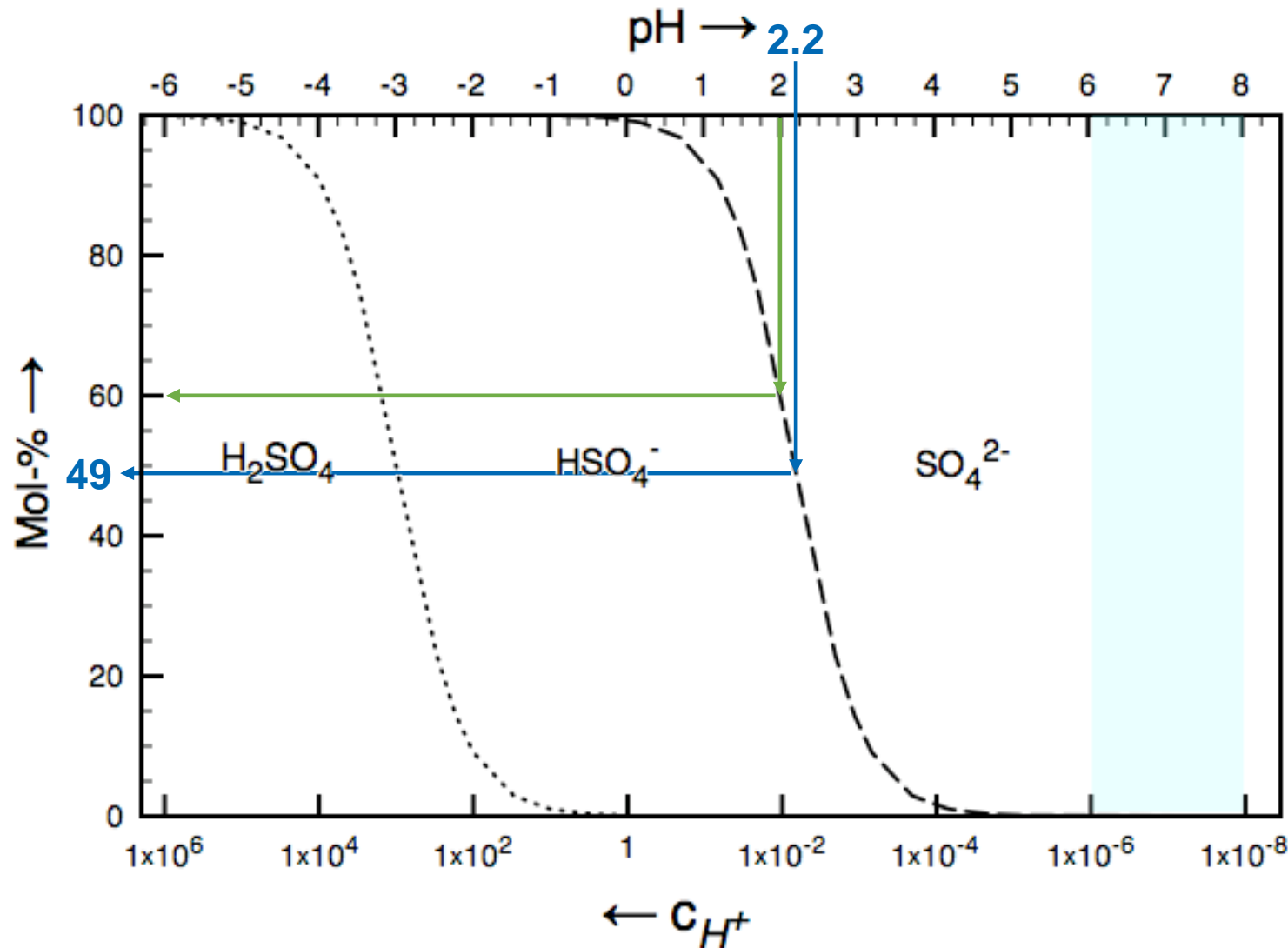
$c(\text{HA})$ ... concentration of the associated acid ( $\text{HSO}_4^-$ )

$$\rightarrow c(\text{HA}) = c(\text{A}^-) / 10^{\text{pH} - \text{p}K_a} = 0.33 \text{ mol/l} / 10^{2.2 - 1.92} = 0,1732 \text{ mol/l} ??? \rightarrow \text{pH } 2,71 ???$$

$$\rightarrow c(\text{HA}) = c(\text{A}^-) / 10^{\text{pH} - \text{p}K_a} = 0.33 \text{ mol/l} / 10^{2.2 - 1.99} = 0,2035 \text{ mol/l} ??? \rightarrow \text{pH } 2,2 ???$$

# Understanding Pep

# preparation of electrolyte solution



pH 2.2 →  
49 Mol-%  $HSO_4^-$  equilibrium to  
51 Mol-%  $SO_4^{2-}$

pH 2.0 →  
60 Mol-%  $HSO_4^-$  equilibrium to  
40 Mol-%  $SO_4^{2-}$

## Example: acidic 0.33 M ammonium sulfate solution (pH ~ 2.2)

- Calculation of ingredient ammonium sulfate (44 g/l)
- Mixing (increased temperature ~50 °C)
- pH (water + 0.33 M ammonium sulfate) ~ 6,3 – 6,4
- Calculation of ingredient sulfuric acid (ca. 5.5 ml 4.8 M sulphuric acid / l)
- Slow dosing of sulfuric acid
- (Calculation of conductance)

lifetime:

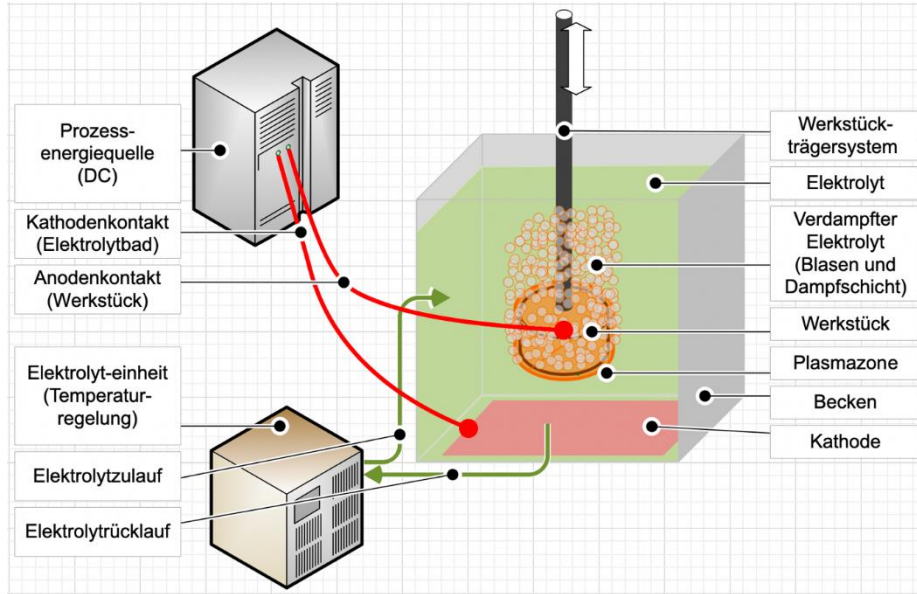
- counted in the amount of charge as a value for how much metal is solved in electrolyte
- ends when required needs could not be achieved any more (gloss/roughness or low MMR)
- mostly first gloss requirements could not be achieved but material removal is still given

refreshing:

- bring out metal elements by taking him the ability to solve them, e.g. change it's pH value → different metal compounds precipitate from the solution
- flocculating agent are helpfull to increase the agglomeration of small partikels
- sedimentation + decantig or filtering
- add required substances to bring it back to ist initial state (pH value)

Safety issue	Precaution
Hydrogen gas formation on the cathode	Gas exhaustion system
Hot electrolyte	Heat resistant work cloths
Chemical hazard	Safety glasses, gloves, lab coat, other equipment
Direct voltage	Electrical insulation
Halides are oxidised during PEP	Filtration system built-in in the gas exhaust system
Consumed electrolyte	Should be disposed according to the environmental safety requirements, i.e. cannot enter wastewater system

# Understanding Pep



## environmental and user safety

